#### **GATHERING COMPANY**

November 5, 2019

Part 70 Program
Environmental Programs Division
Air Quality Program
P.O. Box 737 MS #84
Ignacio, CO 81137

Via email: airquality@southernute-nsn.gov

RE: Part 70 Operating Permit Renewal Application Red Cedar Gathering Company, South Ignacio Central Delivery Point

On April 25, 2019, Red Cedar submitted to EPA a request to revise permit #SMNSR-SU-000013-2016.003 for the South Ignacio Central Delivery Point. The EPA has not provided Red Cedar with a specific date by which they expect to finalize the revised synthetic minor new source review permit for the facility. However, they have verbally informed us that they expect to do so prior to January 23, 2020, which is the date the facility's part 70 operating permit renewal application is due. After conversations with EPA regarding the timing of issuance of the revised SMSNR permit and that it's delay may require us to submit two complete part 70 renewal applications, one prior to SMSNR finalization and then another after, EPA recommended we prepare the renewal application with our requested revisions in place.

Therefore, this part 70 operating permit renewal application incorporates the revisions we requested to the facility's SMSNR permit and includes the following materials:

#### Materials

- Forms CTAC, GIS, EUD-1, EMISS, PTE, and IE;
- Regulatory Applicability Analysis; and
- Supporting documentation.

Should you have any questions or need additional information, please do not hesitate to contact me at (970) 764-6921.

Sincerely,

RED CEDAR GATHERING COMPANY

Kyle Hunderman

Environmental Compliance Specialist II - Air Quality

Cc: US EPA, Region 8, via email: r&airreportenforcement@epa.gov



## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



## FORM CTAC - CERTIFICATION OF TRUTH, ACCURACY, AND COMPLETENESS BY RESPONSIBLE OFFICIAL

INSTRUCTIONS: One copy of this form must be completed, signed and sent with each submission of documents (i.e., application forms, updates to applications, reports, or any information required by part 70 permit).

Company Name: Red Cedar Gathering Company Facility Name: South Ignacio Central Delivery Point

A. Responsible Official			Facility ID: 08-067-U	0033
Name: (Last)	Hadrick	(First)	Kourtney	(MI)
Title:	President – Chief Operating C	)fficer		
Mailing Address:	125 Mercado Street, Suite 20	1		
City:	Durango	State: CO	Zip Code: <u>81</u> :	301
Telephone:	(970) 764-6900 Ext.	Email;	khadrick1@redced	argathering.com
B. Certification of Trut	h, Accuracy and Completeness			
Instructions: This form	n must be signed by the responsible	official		
	of law that, based on information and iments are true, accurate and complete		ter reasonable inquiry, th	e statements and information
Name (signed):	Sourtney Al			
Name (typed):	Kourtney Hadrick		Date:	11-5-19

FORM GIS March 2012



A. Mailing Address and Contact Information

## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



#### APPLICATION FORM GIS - GENERAL INFORMATION AND SUMMARY

Facility Name: South Ignacio Central Delivery Point	Facility ID: 08-067-U0033
Mailing Address: 125 Mercado Street; Suite 201	
City: Durango State: CO	Zip Code: 81301
Contact Person: Kyle Hunderman	Environmental Compliance Specialist II- Air Quality
Telephone: (970) 764-6921 Ext	Email:
B. Facility Location Temporary Source:   Yes  No	
Plant Site Location:	
City: Durango County: La Plata	
<b>Legal Description:</b> Section: 32 Township: 33N Range: 7W Co	ordinates Lat.: 37.053917 Long.: -107.625222
Land Status of Facility Location:	Allotment Other:
Is the facility within 50 miles of:	
Federal Class 1 areas?	Mesa Verde NP Weminuche Wilderness Area
Affected States? ⊠Colorado ⊠New Mexico □Utah	□Ute Mtn. Ute □Navajo □Jicarilla
C. Owner	
Name: Red Cedar Gathering Company	Telephone: 970-764-6900 Ext.
Mailing Address: 125 Mercado Street; Suit 201	
City: Durango State: CO	Zip Code: 8131
D. Operator	■Same as Owner
Name:	Telephone: Ext
Mailing Address:	
City: State:	Zip Code:

FORM GIS March 2012

E. Application Type  Instructions: Mark only one permit application type and en	nter the appropriate date if requested.	
☐Initial Permit, date operations commenced:	07/2	3/2020
Significant Mod	Group Processing, MPM Administrative	e Amendment
F. Applicable Requirement Summary		
Instructions: Mark all that apply.		
□FIP/TIP □PSD □NESHAP □Sec. 112(c	d) MACT Sec. 112(g) MACT Sec. 112(j) MA	СТ
■Federal Minor NSR ■CAA Section 111 ■	RMP [Sec. 112(r)]	reduction of HAP
□Non-attainment NSR □Phase I acid rain □	Phase II acid rain	183(f)
Section 129 Standards/Requirements Consumer/	Commercial products section 183(e)	
NAAQS, increments or visibility (temporary sources)	)	
Has a risk management plan been registered?	Yes No If so, with which regulatory agency:	
Has a phase II acid rain application been submitted?	Yes No If so, with which permitting authority:	<del></del>
G. Source-Wide PTE Restrictions and Applicable Req	uirements	
Instructions: Cite and describe any emissions-limiting req identical fashion to all the sources at the facility. Include a applicable.	uirements that apply to the facility as a whole, or that app	
Unit E1 NOx emissions shall not exceed 9.2 II	b/hr and 40.3 tons per year	
Unit E1 CO emissions shall not exceed 12.9 II	b/hr and 56.5 tons per year	
H. Process Description		
Instructions: List all processes, products, and SIC codes for and SIC codes associated with any alternative operating so narrative description of all facility operations as an attachr	cenarios, if different from those listed for normal operation	
Process	Products	SIC
compress and dehydrate natural gas	medium pressure natural gas	4922

FORM GIS March 2012

#### I. Emission Unit Identification

Instructions: Assign an emissions unit ID and describe each significant emissions unit at the facility. Control equipment and/or alternative operating scenarios associated with emissions units should be included in the description. **Emission Unit ID** Description of Unit E1 Waukesha L7044GSI 4SRB natural gas-fired SI RICE w/ NSCR catalyst E2 Waukesha L7042GL 4SLB natural gas-fired SI RICE E3 Waukesha L7042GL 4SLB natural gas-fired SI RICE E4 Waukesha L7042GL 4SLB natural gas-fired SI RICE E5 Waukesha L5794LT 4SLB natural gas-fired SI RICE w/ oxidation catalyst E6 Waukesha L5794LT 4SLB natural gas-fired SI RICE w/ oxidation catalyst E7 Waukesha L5794LT 4SLB natural gas-fired SI RICE w/ oxidation catalyst E8 Waukesha L5794LT 4SLB natural gas-fired SI RICE w/ oxidation catalyst A. Facility Emissions Summary

Instructions: Enter the uncon	trolled and controlled n	otential to emit (PTE) for t	he facility for each air polluta	int listed below.
		(= ===) 101 1		
Uncontrolled PTE				
NO <sub>x</sub> : 212.5 tons/yr	VOC:tons/yr	$SO_2$ :tons/yr	PM <sub>10</sub> : <b>4.4</b> tons/yr	CO:tons/yr
Lead: 0tons/yr	GHGs (mass-	based):tons/yr	GHGs (CO <sub>2</sub> -equi	valent):tons/yr
Total HAP: 25.3 tons/yr		Single HAP emitted in gr	eatest amount:	PTE: 17.8 tons/yr
Controlled PTE (federally	enforceable)			
NO <sub>x</sub> :tons/yr	VOC:tons/yr	SO <sub>2</sub> :tons/yr	PM <sub>10</sub> :tons/yr	CO:tons/yr
Lead:tons/yr	GHGs (mass-	based):tons/yr	GHGs (CO <sub>2-</sub> equi	valent):tons/yr
Total HAP:tons/yr		Single HAP emitted in gr	reatest amount:	PTE:tons/yr
K. Existing Federally Enfo	rceable Air Permits			□N/A
Permit number: V-SUIT-0	0031-2015.02 Pen	Part 70 Operating Perm	Permitting Authority:	QP

# L. Additional Information Required

Permit number:

Permit number:\_\_

- 1) Attach a site map for the facility
- 2) Attach a complete process flow diagram for the facility which labels all emission units with their assigned emission unit IDs.

Permit type:

Permit type:\_

Permitting Authority: AQP

Permitting Authority:\_\_EPA

Permitting Authority:\_\_\_

- 3) Provide driving directions to the facility.
- 4) Provide a description of safety requirements for visitors.

SMNSR-SU-000043-2015.002

- Provide an updated construction and permitting history of the facility, including the PTE, controlled and uncontrolled, at each 5) stage of construction.
- Attach copies of any cross-referenced documents.
- Provide supporting documentation for the PTE of all pollutants, including the source of emission factors, any available copies of manufacturer's specifications, copies of guarantees for control reduction efficiencies, and emission calculations.



INSTRUCTIONS:

## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



# FORM EUD-1 - EMISSIONS UNIT DESCRIPTION FOR INTERNAL COMBUSTION SOURCES

Facility Name: South Ignacio Central Delivery Point	Facility ID:	08-067-U0033
A. General Information		
Emissions unit ID: E1	Description:	4GSI 4SRB natural gas-fired SI RICE
Primary use: Compress natural gas		
Emergency Use: Yes No Temporary source:	Yes •No Max. A	Annual Operating Hours: 8760
Installation Date:	Ma	mufacture Date:03/01/2003
Order Date from Manufacturer:03/01/2003	Modification or Reco	nstruction Date:
Standard Industrial Classification (4-digit SIC Code): 4	Source Classification	1 Code (8-digit SCC Code):
B. Emission Unit Description		
Manufacturer: Waukesha M	odel No.: L7044GSI	Serial No.: C-14529/1
ENGINES & GENERATOR	RS	TURBINES
Manufacturer Certified? Yes No  Maximum rated heat input capacity (MMBtu/hr): 13.2  Fuel Consumption (Btu/bhp-hr): 7881	2	Turbine Type: Simple Cycle Regenerative Combined Cycle
Name Plate Rating   Horsepower: 1680   Horsepower:		Maximum rated heat input capacity (MMBtu/hr):
Check All That Apply:  Lean Burn  4 - Stroke Cycle  Spark Ignited  Fuel Injected  Turbocharged  Intercooled (IC)	on Ignited	Check All That Apply:  □Lean Premix Gas-fired □Lean Premix Oil-fired □Diffusion Flame Gas-fired □Diffusion Flame Oil-fired

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C. Fuel Data			
Primary Fuel Type:	Natural Gas	Back-up Fuel Type: N/A	
Heat Content (Btu/lb, gal, or scf)	900 btu/scf	Heat Content (BTU/lb, gal, or scf):	
Max. Sulfur Content (%):	0.0	Max. Sulfur Content (%):	
Max. Ash Content (%):	0.0	Max. Ash Content (%):	
Max. Annual Fuel Usage Rate:	128.5 mmscf/yr	Max. Annual Fuel Usage Rate:	
Max. Hourly Fuel Usage Rate:	0.01 mmscf/yr	Max. Hourly Fuel Usage Rate:	
Actual Annual Fuel Usage Rate:	128.5 mmscf/yr	Actual Annual Fuel Usage Rate:	
(Note: Rates should be reported a	as follows: Solid in tons/	yr, Liquid in gal/yr, Gaseous in MMscf/yr)	
D. Associated Air Pollution Cont	eal Vaninmant		N/A
D. Associated An Tonution Cont.	or requipment		IN/A
Device type: NSCR Catalyst	Oxidation Catalyst	Other (describe):	
Manufacturer:	Model N	Io.: Serial No.:	
Installation date or last modifical	tion date:	Air/Fuel Ratio Controller? Yes No	
Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)	Control Efficiency: NOx	(~80%), CO (~68%)	
		ceable emission limit	
Efficiency estimation method:			
E. Additional Information Requi			
On separate sheets of paper include	the following:		
Engine, Turbine, or Generator M pollutant specific emission factor		and site emission estimates/guaranteed	
2. Manufacturer specifications for	any identified air pollutio	on control units and pollution control guarantees.	
•	•		m NY/A
F. Ambient Impact Assessment		<u> </u>	■ N/A
Instructions: This information m common).	ust be completed when a	an ambient impact assessment is required for this emissions unit (this	s is not
Stack heig	ght (ft):	Inside stack diameter (ft):	

Stack temp (°F):

Actual stack flow rate (ACFM):

Design stack flow rate (ACFM):

Velocity (ft/sec):



INSTRUCTIONS:

## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



# FORM EUD-1 - EMISSIONS UNIT DESCRIPTION FOR INTERNAL COMBUSTION SOURCES

Facility Name: South Ignacio Central Delivery Point	Facility ID:	08-067-U0033
A. General Information		
Emissions unit ID: <u>E2</u>	Description: Waukesha L704	42GL 4SLB natural gas-fired SI RICE
Primary use: Compress natural gas		
Emergency Use: Yes No Temporary source	ce: Yes No Max. A	Annual Operating Hours: 8760
Installation Date:		anufacture Date:
Order Date from Manufacturer: 10/21/1996	Modification or Reco	onstruction Date:
Standard Industrial Classification (4-digit SIC Code	): 4922 Source Classification	n Code (8-digit SCC Code):
B. Emission Unit Description		
Manufacturer: Waukesha	Model No.: L7042GL	Serial No.: C-12215/4
ENGINES & GENERAT	TORS	TURBINES
Manufacturer Certified? Yes No  Maximum rated heat input capacity (MMBtu/hr): 9  Fuel Consumption (Btu/bhp-hr): 7284	.7	Turbine Type:  Simple Cycle Regenerative Combined Cycle
1	Site Rating ver: 1337 nm): 1200	Maximum rated heat input capacity (MMBtu/hr):
■Fuel Injected ■Carbur	oke Cycle ession Ignited eted Ily Aspirated	Check All That Apply:  □Lean Premix Gas-fired □Lean Premix Oil-fired □Diffusion Flame Gas-fired □Diffusion Flame Oil-fired

		X X & X X X X X X X X X X X X X X X X X	ch 2012
C. Fuel Data			
Primary Fuel Type:	Natural Gas	Back-up Fuel Type: N/A	
Heat Content (Btu/lb, gal, or scf):	900 btu/scf	Heat Content (BTU/lb, gal, or scf):	
Max. Sulfur Content (%):	0.0	Max. Sulfur Content (%):	
Max. Ash Content (%):	0.0	Max. Ash Content (%):	
Max. Annual Fuel Usage Rate:	94.4 mmscf/yr	Max. Annual Fuel Usage Rate:	
Max. Hourly Fuel Usage Rate:	0.01 mmscf/yr	Max. Hourly Fuel Usage Rate:	
Actual Annual Fuel Usage Rate:	94.4 mmscf/yr	Actual Annual Fuel Usage Rate:	
(Note: Rates should be reported as	s follows: Solid in tons/y	r; Liquid in gal/yr, Gaseous in MMscf/yr)	
D. Associated Air Pollution Contr	ol Equipment		■N/A
Device type: NSCR Catalyst	Oxidation Catalyst	Other (describe):	
Manufacturer:	Model No	o.: Serial No.:	
Manufacturer: Installation date or last modificat		p	
Installation date or last modificat  Air Pollutant(s) Controlled and C	ion date:	p	
Installation date or last modificat Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)	ion date:	Air/Fuel Ratio Controller? Yes	
Installation date or last modificat Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)	ion date:	Air/Fuel Ratio Controller? Yes	
Installation date or last modificat Air Pollutant(s) Controlled and C  Example: CO (90%), VOC (45%)  Efficiency estimation method:	ion date:	Air/Fuel Ratio Controller? Yes	
Installation date or last modificat Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)  Efficiency estimation method:  E. Additional Information Requir	ion date:	Air/Fuel Ratio Controller? Yes	
Installation date or last modificat Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)  Efficiency estimation method:  E. Additional Information Requir On separate sheets of paper include	ced the following:	Air/Fuel Ratio Controller? Yes	
Installation date or last modificat Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)  Efficiency estimation method:  E. Additional Information Requir On separate sheets of paper include	ion date: Control Efficiency:  Control Efficiency:	Air/Fuel Ratio Controller? Yes	
Installation date or last modificat Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)  Efficiency estimation method:  E. Additional Information Requir On separate sheets of paper include  1. Engine, Turbine, or Generator M pollutant specific emission factor	control Efficiency:  Ted the following:  Ianufacturer's site rating are.	Air/Fuel Ratio Controller? Yes	
Installation date or last modificat Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)  Efficiency estimation method:  E. Additional Information Requir On separate sheets of paper include  1. Engine, Turbine, or Generator M pollutant specific emission factor	control Efficiency:  Ted the following:  Ianufacturer's site rating are.	Air/Fuel Ratio Controller? Yes and site emission estimates/guaranteed	No
Installation date or last modificat Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)  Efficiency estimation method:  E. Additional Information Requir On separate sheets of paper include  1. Engine, Turbine, or Generator M pollutant specific emission factor	control Efficiency:  Ted the following:  Ianufacturer's site rating are.	Air/Fuel Ratio Controller? Yes and site emission estimates/guaranteed	

Stack height (ft):

Stack temp (°F):

Actual stack flow rate (ACFM):

Inside stack diameter (ft):

Velocity (ft/sec):

Design stack flow rate (ACFM):



INSTRUCTIONS:

## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70 $\,$



# FORM EUD-1 - EMISSIONS UNIT DESCRIPTION FOR INTERNAL COMBUSTION SOURCES

Facility Name: South Ignacio Central Delivery Point	Facility ID:	08-067-U0033
A. General Information		
Emissions unit ID: E3	Description: Waukesha L704	42GL 4SLB natural gas-fired SI RICE
Primary use: Compress natural gas		
Emergency Use: Yes No Temporary source	e: Yes •No Max. A	Annual Operating Hours: 8760
Installation Date:		anufacture Date:
Order Date from Manufacturer: 04/01/1991	Modification or Reco	onstruction Date:
Standard Industrial Classification (4-digit SIC Code)	Source Classification	n Code (8-digit SCC Code): 20200254
B. Emission Unit Description		
Manufacturer: Waukesha	Model No.: L7042GL	Serial No.: 403301
ENGINES & GENERAT	ORS	TURBINES
Manufacturer Certified? Yes No  Maximum rated heat input capacity (MMBtu/hr): 9  Fuel Consumption (Btu/bhp-hr): 7284	7	Turbine Type:  ☐Simple Cycle ☐Regenerative ☐Combined Cycle
1	Site Rating ver: 1337 m): 1200	Maximum rated heat input capacity (MMBtu/hr):
Fuel Injected Carbure	ske Cycle ession Ignited eted lly Aspirated	Check All That Apply:  □Lean Premix Gas-fired □Lean Premix Oil-fired □Diffusion Flame Gas-fired □Diffusion Flame Oil-fired

FORM EUD-1			March 2012
C. Fuel Data			
Primary Fuel Type:	Natural Gas	Back-up Fuel Type: N/A	•••••
Heat Content (Btu/lb, gal, or scf)	900 btu/scf	Heat Content (BTU/lb, gal, or scf):	
Max. Sulfur Content (%):	0.0	Max. Sulfur Content (%):	
Max. Ash Content (%):	0.0	Max. Ash Content (%):	
Max. Annual Fuel Usage Rate:	94.4 mmscf/yr	Max. Annual Fuel Usage Rate:	
Max. Hourly Fuel Usage Rate:	0.01 mmscf/yr	Max. Hourly Fuel Usage Rate:	
Actual Annual Fuel Usage Rate:	94.4 mmscf/yr	Actual Annual Fuel Usage Rate:	
(Note: Rates should be reported a	ns follows: Solid in tons/yr	r, Liquid in gal/yr, Gaseous in MMscf/yr)	
D. Associated Air Pollution Cont	rol Equipment		■N/A
Device type: NSCR Catalyst		Other (describe):	
Manufacturer:		.: Serial No.:	
Installation date or last modifica	tion date:	Air/Fuel Ratio Controller? • Yes	s <b>I</b> No
Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)			······
Efficiency estimation method:			
E. Additional Information Requi			
	-		
Engine, Turbine, or Generator N     pollutant specific emission factor		nd site emission estimates/guaranteed	
2. Manufacturer specifications for	any identified air pollution	control units and pollution control guarantees.	
			■N/A
F. Ambient Impact Assessment Instructions: This information macommon).	nust be completed when an	ambient impact assessment is required for this emission	s unit (this is not

Stack height (ft):

Stack temp (°F):

Actual stack flow rate (ACFM):

Inside stack diameter (ft):

Velocity (ft/sec):

Design stack flow rate (ACFM):



INSTRUCTIONS:

## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



# FORM EUD-1 - EMISSIONS UNIT DESCRIPTION FOR INTERNAL COMBUSTION SOURCES

Facility Name: South Ignacio Central Delivery Point	Facility ID:	08-067-U0033
A. General Information		
Emissions unit ID:	Description: Waukesha L704	12GL 4SLB natural gas-fired SI RICE
Primary use: Compress natural gas		
Emergency Use: Yes No Temporary source	:: Yes •No Max. A	Annual Operating Hours: 8760
Installation Date:	Ma	nnufacture Date:07/01/1996
Order Date from Manufacturer:07/01/1996	Modification or Reco	nstruction Date:
Standard Industrial Classification (4-digit SIC Code):	4922 Source Classification	Code (8-digit SCC Code):
B. Emission Unit Description		
Manufacturer: Waukesha	Model No.: L7042GL	Serial No.: C-12097/1
ENGINES & GENERATO	ORS	TURBINES
Manufacturer Certified? Yes No  Maximum rated heat input capacity (MMBtu/hr): 9.  Fuel Consumption (Btu/bhp-hr): 7284	7	Turbine Type: Simple Cycle Regenerative Combined Cycle
1	Site Rating or: 1337 a): 1200	Maximum rated heat input capacity (MMBtu/hr):
■Fuel Injected ■Carbure	te Cycle ssion Ignited ted y Aspirated	Check All That Apply:  □Lean Premix Gas-fired □Lean Premix Oil-fired □Diffusion Flame Gas-fired □Diffusion Flame Oil-fired

FORM EUD-1		March 1	2012
C. Fuel Data			
Primary Fuel Type:	Natural Gas	Back-up Fuel Type: N/A	
Heat Content (Btu/lb, gal, or scf):	900 btu/scf	Heat Content (BTU/lb, gal, or scf):	
Max. Sulfur Content (%):	0.0	Max. Sulfur Content (%):	
Max. Ash Content (%):	0.0	Max. Ash Content (%):	
Max. Annual Fuel Usage Rate:	94.4 mmscf/yr	Max. Annual Fuel Usage Rate:	
Max. Hourly Fuel Usage Rate:	0.01 mmscf/yr	Max. Hourly Fuel Usage Rate:	
Actual Annual Fuel Usage Rate:	94.4 mmscf/yr	Actual Annual Fuel Usage Rate:	
(Note: Rates should be reported a	s follows: Solid in tons/	yr, Liquid in gal/yr, Gaseous in MMscf/yr)	
D. Associated Air Pollution Conti	rol Equipment		■ N/A
p			
Device type: NSCR Catalyst	Oxidation Catalyst	Other (describe):	
Manufacturer:	Model N	Io.: Serial No.:	
Installation date or last modificat	ion date:	Air/Fuel Ratio Controller? Yes No	
Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)	Control Efficiency:		
Efficiency estimation method:			
E. Additional Information Requir	rod .		
On separate sheets of paper include			
Engine, Turbine, or Generator M pollutant specific emission facto		and site emission estimates/guaranteed	
2. Manufacturer specifications for	any identified air pollution	on control units and pollution control guarantees.	
			■ N/A
F Amhient Impact Accessment			

<b>F. Ambient Impact Assessment</b> Instructions: This information must be completed when an common).	n ambient impact assessment is required for this emissions unit (this is not
Stack height (ft):	Inside stack diameter (ft):
Stack temp (°F):	Design stack flow rate (ACFM):
Actual stack flow rate (ACFM):	Velocity (ft/sec):



INSTRUCTIONS:

## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



# FORM EUD-1 - EMISSIONS UNIT DESCRIPTION FOR INTERNAL COMBUSTION SOURCES

Facility Name: South Ignacio Central Delivery Point Facility II	D: 08-067-U0033
A. General Information	
Emissions unit ID: E5 Description: Waukesha L5	5794LT 4SLB natural gas-fired SI RICE
Primary use: Compress natural gas	
Emergency Use: Yes No Temporary source: Yes No Max	. Annual Operating Hours: 8760
Installation Date: 08/24/2007	Manufacture Date: 02/01/2006
02/01/2006	construction Date:
Standard Industrial Classification (4-digit SIC Code): 4922 Source Classification	ion Code (8-digit SCC Code): 20200254
B. Emission Unit Description	
Manufacturer: Waukesha Model No.: L5794LT	Serial No.: <u>C-15962/1</u>
ENGINES & GENERATORS	TURBINES
Manufacturer Certified? Yes No  Maximum rated heat input capacity (MMBtu/hr): 10.6  Fuel Consumption (Btu/bhp-hr): 7600	Turbine Type: Simple Cycle Regenerative Combined Cycle
Name Plate Rating   Site Rating	Maximum rated heat input capacity (MMBtu/hr):
Check All That Apply:  Lean Burn  4 - Stroke Cycle  Spark Ignited  Fuel Injected  Turbocharged  Intercooled (IC)	Check All That Apply:  □Lean Premix Gas-fired □Lean Premix Oil-fired □Diffusion Flame Gas-fired □Diffusion Flame Oil-fired

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C. Fuel Data			
Primary Fuel Type:	Natural Gas	Back-up Fuel Type: N/A	
Heat Content (Btu/lb, gal, or scf):	900 btu/scf	Heat Content (BTU/lb, gal, or scf):	_
Max. Sulfur Content (%):	0.0	Max. Sulfur Content (%):	···
Max. Ash Content (%):	0.0	Max. Ash Content (%):	
Max. Annual Fuel Usage Rate:	103.6 mmscf/yr	Max. Annual Fuel Usage Rate:	<del></del>
Max. Hourly Fuel Usage Rate:	0.01 mmscf/yr	Max. Hourly Fuel Usage Rate:	_
Actual Annual Fuel Usage Rate:	103.6 mmscf/yr	Actual Annual Fuel Usage Rate:	
(Note: Rates should be reported a	s follows: Solid in tons/yr;	Liquid in gal/yr, Gaseous in MMscf/yr)	
D. Associated Air Pollution Contr	ral Faninment		N/A
Device type: NSCR Catalyst	Oxidation Catalyst	Other (describe):	-
Manufacturer:	Model No.:	Serial No.:	<b>-</b>
Installation date or last modificat	ion date:	Air/Fuel Ratio Controller? Yes No	0
Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)	Control Efficiency: CO (9	3%)	
Efficiency estimation method:	Emission test data	a	•
Efficiency estimation method:			-
E. Additional Information Requir			
On separate sheets of paper include	the following:		
Engine, Turbine, or Generator M.     pollutant specific emission facto	-	nd site emission estimates/guaranteed	
2. Manufacturer specifications for a	any identified air pollution	control units and pollution control guarantees.	
		V	- NY/A
F. Ambient Impact Assessment			■ N/A
-	ust be completed when an a	ambient impact assessment is required for this emissions unit (t	his is not
Stack heig	 ght (ft):	Inside stack diameter (ft):	

Stack temp (°F): \_\_\_\_\_ Design stack flow rate (ACFM): \_\_\_\_\_

Actual stack flow rate (ACFM):

Velocity (ft/sec):



INSTRUCTIONS:

## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



# FORM EUD-1 - EMISSIONS UNIT DESCRIPTION FOR INTERNAL COMBUSTION SOURCES

Facility Name: South Ignacio Central Delivery Poin	t Facility ID:	08-067-U0033
A. General Information		
Emissions unit ID:	Description: Waukesha L57	94LT 4SLB natural gas-fired SI RICE
Primary use: Compress natural gas		
Emergency Use: Yes No Temporary sou	ırce: Yes •No Max. A	Annual Operating Hours: 8760
Installation Date:		anufacture Date:11/01/2005
Order Date from Manufacturer:11/01/2005		onstruction Date:
Standard Industrial Classification (4-digit SIC Cod		n Code (8-digit SCC Code):
B. Emission Unit Description		
Manufacturer: Waukesha	Model No.: L5794LT	Serial No.: C-16161/1
ENGINES & GENERA	TORS	TURBINES
Manufacturer Certified? Yes No  Maximum rated heat input capacity (MMBtu/hr):  Fuel Consumption (Btu/bhp-hr): 7600	10.6	Turbine Type: Simple Cycle Regenerative Combined Cycle
	Site Rating ower: 1401 rpm): 1200	Maximum rated heat input capacity (MMBtu/hr):
■Spark Ignited ■Comp ■Fuel Injected ■Carbu	roke Cycle pression Ignited ureted rally Aspirated	Check All That Apply:  Lean Premix Gas-fired  Lean Premix Oil-fired  Diffusion Flame Gas-fired  Diffusion Flame Oil-fired

A GARAGE MACOLAN A		7.1 AAAA AAA	7 W C A AW
C. Fuel Data			
Primary Fuel Type:	Natural Gas	Back-up Fuel Type: N/A	
Heat Content (Btu/lb, gal, or scf):	900 btu/scf	Heat Content (BTU/lb, gal, or scf):	_
Max. Sulfur Content (%):	0.0	Max. Sulfur Content (%):	···
Max. Ash Content (%):	0.0	Max. Ash Content (%):	
Max. Annual Fuel Usage Rate:	103.6 mmscf/yr	Max. Annual Fuel Usage Rate:	<del></del>
Max. Hourly Fuel Usage Rate:	0.01 mmscf/yr	Max. Hourly Fuel Usage Rate:	_
Actual Annual Fuel Usage Rate:	103.6 mmscf/yr	Actual Annual Fuel Usage Rate:	
(Note: Rates should be reported a	s follows: Solid in tons/yr;	Liquid in gal/yr, Gaseous in MMscf/yr)	
D. Associated Air Pollution Contr	ral Faninment		N/A
Device type: NSCR Catalyst	Oxidation Catalyst	Other (describe):	-
Manufacturer:	Model No.:	Serial No.:	<b>-</b>
Installation date or last modificat	ion date:	Air/Fuel Ratio Controller? Yes No	0
Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)	Control Efficiency: CO (9	3%)	
Efficiency estimation method:	Emission test data	a	•
Efficiency estimation method:			-
E. Additional Information Requir			
On separate sheets of paper include	the following:		
Engine, Turbine, or Generator M.     pollutant specific emission facto	-	nd site emission estimates/guaranteed	
2. Manufacturer specifications for a	any identified air pollution	control units and pollution control guarantees.	
		V	- NY/A
F. Ambient Impact Assessment			■ N/A
-	ust be completed when an a	ambient impact assessment is required for this emissions unit (t	his is not
Stack heig	 ght (ft):	Inside stack diameter (ft):	

Stack temp (°F): \_\_\_\_\_ Design stack flow rate (ACFM): \_\_\_\_\_

Actual stack flow rate (ACFM):

Velocity (ft/sec):



INSTRUCTIONS:

## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



# FORM EUD-1 - EMISSIONS UNIT DESCRIPTION FOR INTERNAL COMBUSTION SOURCES

Facility Name: South Ignacio Central	Delivery Point Facility	· ID: 08-067-U0033
A. General Information		
Emissions unit ID: <b>E7</b>	Description: Waukesha L	L5794LT 4SLB natural gas-fired SI RICE
Primary use: Compress nate	ural gas	
Emergency Use: Yes •No	Γemporary source: ☐Yes ■No Ma	ax. Annual Operating Hours: 8760
Installation Date:	03/29/2006	Manufacture Date: 09/12/2005
Order Date from Manufacturer:	09/12/2005 Modification or F	Reconstruction Date:
Standard Industrial Classification (4	-digit SIC Code): 4922 Source Classifica	ation Code (8-digit SCC Code):
B. Emission Unit Description		
Manufacturer: Waukesha	Model No.: L5794LT	Serial No.: <u>C-15838/1</u>
ENGINES	& GENERATORS	TURBINES
Manufacturer Certified? Yes  Maximum rated heat input capacity	(MMBtu/hr): 10.6	Turbine Type: Simple Cycle Regenerative Combined Cycle
Fuel Consumption (Btu/bhp-hr): 76  Name Plate Rating Horsepower: 1447	Site Rating  Horsepower: 1401	Maximum rated heat input capacity (MMBtu/hr):
Speed (rpm): 1200	Speed (rpm): 1200	
Check All That  Lean Burn  4 - Stroke Cycle Spark Ignited Fuel Injected Turbocharged Intercooled (IC)	Apply:  Rich Burn  2 - Stroke Cycle Compression Ignited Carbureted Naturally Aspirated Dual Fuel	Check All That Apply:  □Lean Premix Gas-fired □Lean Premix Oil-fired □Diffusion Flame Gas-fired □Diffusion Flame Oil-fired

A GARAGE MACOLAN A		7.1 AAAA AAA	7 W C A AW
C. Fuel Data			
Primary Fuel Type:	Natural Gas	Back-up Fuel Type: N/A	
Heat Content (Btu/lb, gal, or scf):	900 btu/scf	Heat Content (BTU/lb, gal, or scf):	_
Max. Sulfur Content (%):	0.0	Max. Sulfur Content (%):	···
Max. Ash Content (%):	0.0	Max. Ash Content (%):	
Max. Annual Fuel Usage Rate:	103.6 mmscf/yr	Max. Annual Fuel Usage Rate:	<del></del>
Max. Hourly Fuel Usage Rate:	0.01 mmscf/yr	Max. Hourly Fuel Usage Rate:	_
Actual Annual Fuel Usage Rate:	103.6 mmscf/yr	Actual Annual Fuel Usage Rate:	
(Note: Rates should be reported a	s follows: Solid in tons/yr;	Liquid in gal/yr, Gaseous in MMscf/yr)	
D. Associated Air Pollution Contr	ral Faninment		N/A
Device type: NSCR Catalyst	Oxidation Catalyst	Other (describe):	-
Manufacturer:	Model No.:	Serial No.:	<b>-</b>
Installation date or last modificat	ion date:	Air/Fuel Ratio Controller? Yes No	0
Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)	Control Efficiency: CO (9	3%)	
Efficiency estimation method:	Emission test data	a	•
Efficiency estimation method:			-
E. Additional Information Requir			
On separate sheets of paper include	the following:		
Engine, Turbine, or Generator M.     pollutant specific emission facto	-	nd site emission estimates/guaranteed	
2. Manufacturer specifications for a	any identified air pollution	control units and pollution control guarantees.	
		V	- NY/A
F. Ambient Impact Assessment			■ N/A
-	ust be completed when an a	ambient impact assessment is required for this emissions unit (t	his is not
Stack heig	 ght (ft):	Inside stack diameter (ft):	

Stack temp (°F): \_\_\_\_\_ Design stack flow rate (ACFM): \_\_\_\_\_

Actual stack flow rate (ACFM):

Velocity (ft/sec):



INSTRUCTIONS:

## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70 $\,$



# FORM EUD-1 - EMISSIONS UNIT DESCRIPTION FOR INTERNAL COMBUSTION SOURCES

Facility Name: South Ignacio Central Delivery Point Facility	ID: 08-067-U0033
A. General Information	
Emissions unit ID: E8 Description: Waukesha L	5794LT 4SLB natural gas-fired SI RICE
Primary use: Compress natural gas	
Emergency Use: Yes No Temporary source: Yes No Ma	x. Annual Operating Hours: 8760
	Manufacture Date:11/03/2005
11/02/2005	econstruction Date:
Standard Industrial Classification (4-digit SIC Code): 4922 Source Classification	tion Code (8-digit SCC Code):
B. Emission Unit Description	
Manufacturer: Waukesha Model No.: L5794LT	Serial No.: <u>C-16160/1</u>
ENGINES & GENERATORS	TURBINES
Manufacturer Certified? Yes No  Maximum rated heat input capacity (MMBtu/hr): 10.6  Fuel Consumption (Btu/bhp-hr): 7600	Turbine Type: Simple Cycle Regenerative Combined Cycle
Name Plate Rating         Site Rating           Horsepower:         1447           Horsepower:         1401           Speed (rpm):         1200           Speed (rpm):         1200	Maximum rated heat input capacity (MMBtu/hr):
Check All That Apply:  □ Lean Burn □ 4 - Stroke Cycle □ Spark Ignited □ Fuel Injected □ Turbocharged □ Intercooled (IC) □ Dual Fuel	Check All That Apply:  □Lean Premix Gas-fired □Lean Premix Oil-fired □Diffusion Flame Gas-fired □Diffusion Flame Oil-fired

C. Fuel Data			
Primary Fuel Type:	Natural Gas	Back-up Fuel Type: N/A	
Heat Content (Btu/lb, gal, or scf):	900 btu/scf	Heat Content (BTU/lb, gal, or scf):	
Max. Sulfur Content (%):	0.0	Max. Sulfur Content (%):	
Max. Ash Content (%):	0.0	Max. Ash Content (%):	
Max. Annual Fuel Usage Rate:	103.6 mmscf/yr	Max. Annual Fuel Usage Rate:	
Max. Hourly Fuel Usage Rate:	0.01 mmscf/yr	Max. Hourly Fuel Usage Rate:	
Actual Annual Fuel Usage Rate:	103.6 mmscf/yr	Actual Annual Fuel Usage Rate:	
(Note: Rates should be reported as	s follows: Solid in tons/yr	Liquid in gal/yr, Gaseous in MMscf/yr)	
D. Associated Air Pollution Contr	ol Equipment		/A
Device type: NSCR Catalyst	Oxidation Catalyst	Other (describe):	
Manufacturer:	Model No.	: Serial No.:	
Installation date or last modification	ion date:	Air/Fuel Ratio Controller? Yes No	
Air Pollutant(s) Controlled and C Example: CO (90%), VOC (45%)	Control Efficiency: CO (9	3%)	
	*minning toot dat		
Efficiency estimation method: "	:mission test dati	3	
Efficiency estimation method:	Emission test data	a	
		a	
E. Additional Information Requir On separate sheets of paper include	red	a	
E. Additional Information Requir On separate sheets of paper include	red the following: Janufacturer's site rating ar		
E. Additional Information Requir On separate sheets of paper include  1. Engine, Turbine, or Generator M pollutant specific emission factor	red the following: Ianufacturer's site rating ar		
E. Additional Information Requir On separate sheets of paper include  1. Engine, Turbine, or Generator M pollutant specific emission factor	red the following: Ianufacturer's site rating ar	nd site emission estimates/guaranteed  control units and pollution control guarantees.	'Α
E. Additional Information Requir On separate sheets of paper include  1. Engine, Turbine, or Generator M pollutant specific emission factor	red the following: Ianufacturer's site rating ar	nd site emission estimates/guaranteed	
E. Additional Information Requirement On separate sheets of paper include  1. Engine, Turbine, or Generator Magnetic pollutant specific emission factor  2. Manufacturer specifications for a pollutant specific emission factor  F. Ambient Impact Assessment	red the following:  Ianufacturer's site rating ares.  any identified air pollution	nd site emission estimates/guaranteed  control units and pollution control guarantees.	

Stack temp (°F): \_\_\_\_\_ Design stack flow rate (ACFM): \_\_\_\_\_

Actual stack flow rate (ACFM):

Velocity (ft/sec):

FORM PTE March 2012



## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



#### APPLICATION FORM PTE - POTENTIAL TO EMIT SUMMARY

INSTRUCTIONS: Complete this form once for the facility. For each significant emissions unit with emissions that count towards applicability, list the emissions unit ID and the PTE (in tons/yr) for the air pollutants listed below. If there are other air pollutants not listed below for which the source is a major source, provide an attachment naming the air pollutant and showing a calculation of the PTE for that pollutant. Provide the combined total for all insignificant emissions units (IEUs) in the specified line below. Round all values to the nearest tenth of a ton. Add all values together in each column and enter the total in the space provided at the bottom of the table. Also report these totals in section **J** of form **GIS**. Attach all supporting documentation for PTE calculations, including emission factors and any enforceable control reduction efficiencies used.

Facility Name: South Ig	nacio Central D	Delivery Point		***************************************	Facili	ty ID: 08-06	7-U0033	***************************************	***************************************
_		Regulated Air Pollutants							
Emissions Unit ID	NO.	VOC	50.	PM.	CO	Lead	HAP	GHGs (Mass-based)	GHGs (CO <sub>3</sub> -equivalent)
E1	40.3	5.8	0.0	1.1	56.5	0.0	1.8		6692.2
E2	19.4	12.9	0.0	0.4	34.9	0.0	3.0		5444.2
E3	19.4	12.9	0.0	0.4	34.9	0.0	3.0		5444.2
E4	19.4	12.9	0.0	0.4	34.9	0.0	3.0		5444.2
E5	28.1	13.5	0.0	0.5	24.9	0.0	3.3		5976.0
E6	28.1	13.5	0.0	0.5	24.9	0.0	3.3		5976.0
E7	28.1	13.5	0.0	0.5	24.9	0.0	3.3		5976.0
E8	29.1	13.5	0.0	0.5	24.9	0.0	3.3		5976.0
	····			·····					
Total IEUs	1.5	2.5	0.0	0.1	1.3	0.0	0.6	<del></del>	7396.5
TOTAL	212.5	101.2	0.0	4.4	261.9	0.0	25.3		54325.1

FORM EMISS March 2012



## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



#### FORM EMISS - EMISSIONS CALCULATIONS

INSTRUCTIONS: Use this form to calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit identified in section I of form GIS. If form FEE does not need to be submitted with the application you do not need to calculate actual emissions. First, list each air pollutant emitted by the unit that is regulated or for which the source is major and then list any other pollutant subject to regulation. Total HAPs may be simply listed as "Total HAP". Individual HAPs should be listed separately if possible. Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each listed air pollutant. Include all fugitives, including those that do not count towards applicability, when calculating actual emissions. At a minimum, round to the nearest tenth of a ton for yearly values or tenth of a pound for hourly values. Attach examples of calculations that illustrate the methodology used.

Facility Name: South Ignacio Central Delivery Point			Emissions Unit	ID: E1
Facility ID: 08-067-U0033		Emission Rati		
Air Pollutants	Actual Annual Emissions (tons/yr)	Poten Hourly (lb/hr)	itial to Emit Annual (tons/yr)	CAS Number
NOx		9.2	40.3	
CO		12.9	56.5	
VOC		1.3	5.8	
НАР		0.4	1.9	
Formaldehyde		0.3	1.2	
CO2e			6692.2	

FORM EMISS March 2012



## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70

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#### FORM EMISS - EMISSIONS CALCULATIONS

INSTRUCTIONS: Use this form to calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit identified in section I of form GIS. If form FEE does not need to be submitted with the application you do not need to calculate actual emissions. First, list each air pollutant emitted by the unit that is regulated or for which the source is major and then list any other pollutant subject to regulation. Total HAPs may be simply listed as "Total HAP". Individual HAPs should be listed separately if possible. Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each listed air pollutant. Include all fugitives, including those that do not count towards applicability, when calculating actual emissions. At a minimum, round to the nearest tenth of a ton for yearly values or tenth of a pound for hourly values. Attach examples of calculations that illustrate the methodology used.

Facility Name: South Ignacio Central Delivery Point	t		Emissions Unit II	<b>D:</b> E2, E3, & E4
Facility ID: 08-067-U0033		Emission Rates Actual Annual Potentia		
Air Pollutants	Actual Annual Emissions (tons/yr)	Hourly (lb/hr)	Annual (tons/yr)	CAS Number
NOx		4.4	19.4	
СО		8.0	34.9	
VOC		2.3	12.9	
HAP		0.7	3.0	
Formaldehyde		0.5	2.2	
CO2e			5444.2	

FORM EMISS March 2012



## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70

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#### FORM EMISS - EMISSIONS CALCULATIONS

INSTRUCTIONS: Use this form to calculate potential to emit (PTE) for applicability purposes and actual emissions for fee purposes for each emissions unit identified in section I of form GIS. If form FEE does not need to be submitted with the application you do not need to calculate actual emissions. First, list each air pollutant emitted by the unit that is regulated or for which the source is major and then list any other pollutant subject to regulation. Total HAPs may be simply listed as "Total HAP". Individual HAPs should be listed separately if possible. Next, calculate PTE for applicability purposes and actual emissions for fee purposes for each listed air pollutant. Include all fugitives, including those that do not count towards applicability, when calculating actual emissions. At a minimum, round to the nearest tenth of a ton for yearly values or tenth of a pound for hourly values. Attach examples of calculations that illustrate the methodology used.

Facility Name: South Ignacio Central Delivery Point	Emissions Unit ID: E5, E6, E7, & E8			
Facility ID: 08-067-U0033		Emission Rate		
Air Pollutants	Actual Annual Emissions (tons/yt)	Hourly (lb/hr)	Annual (tons/yr)	CAS Number
NOx		6.4	28.1	
СО		5.7	24.9	
VOC		3.1	13.5	
HAP		0.8	3.3	
Formaldehyde		0.6	2.5	
CO2e			5976.0	

FORM IE March 2012



## SOUTHERN UTE INDIAN TRIBE - RESERVATION AIR PROGRAM APPLICATION FOR TRIBAL OPERATING PERMIT, 40 CFR PART 70



#### APPLICATION FORM IE - INSIGNIFICANT EMISSIONS

INSTRUCTIONS: List each source of insignificant emissions in the table below. In the "Quantity" column, indicate the number of units qualifying under each description. Each description must be brief but specific enough to describe the source of emissions. List emission units separately if they have dissimilar descriptions, including dissimilar capacities or sizes and other factors. Provide manufacturer emissions specifications, or stack test data when available, including emissions calculations showing that each unit is indeed an insignificant emissions unit.

Facility Name: Sou	th Ignacio Centra	Delivery Point Facility ID: 08-067-U0033
Unit IDs (if available)	Quantity	Description of Activities or Emissions Units
D1	1	30 MMscfd TEG Dehydrator
D2	1	40 MMscfd TEG Dehydrator
TK-501→502	2	Used oil tanks (500 bbl)
TK-503	1	Dehydrator still vent drain tank (95 bbl)
TK-504→511	8	Lube oil storage tanks (500 gal)
TK-512→519	8	Used oil storage tanks (500 gal)
TK-520	1	Ethylene glycol storage tank (500 gal)
TK-521→522	2	TEG storage tanks (500 gal)
RB1	1	1.750 MMBtu/hr TEG dehydrator reboiler heater (D1)
RB2	1	0.750 MMBtu/hr TEG dehydrator reboiler heater (D2)
H-101→102	2	0.325 MMBtu/hr used oil storage tank heaters
H-103	1	0.008 MMBtu/hr catalytic heater
FUG	nna inav	Fugitive emissions

## Applicability Determination

40 CFR Part Description	Applicable Requiremen	Reason
Part 52.21 Prevention of Significant Deterioration	Y	The facility does not belong to any of the 28 source categories. Therefore the potential to emit threshold for determining PSD applicability for the facility is 250 tons of any criteria air pollutant per year and 100,000 tons per year of CO2e. The facility's uncontrolled potential to emit NOx and CO is above major source thresholds; however, it operates under federally enforceable NOx emission limit and is accordingly a synthetic minor NSR source of NOx and a major source of CO. Therefore, the facility is a major NSR source and is subject to 40 CFR part 52.
Part 60 Standards of Performance for New Stationary Sources		Most of the standards set forth by these regulations do not apply to the facility because no applicable units exist at the facility. Specific standards which do not apply at the facility but may apply in general to natural gas production, transmission and/or processing facilities include:
Subpart A General Provisions This rule applies to stationary sources containing an affected facility, the construction or modification of which is commenced after the date of publication in 40 CFR Part 60 of any standard applicable to the facility.	И	As described in the following sections, the facility is not subject to one or more standards of performance for new stationary sources. Therefore the facility is not subject to 40 CFR 60 subpart A.
Subpart Dc Standards of Performance for Small Industrial-Commercial-Institutional Steam Generating Units This rule applies to steam generating units [i.e., a device that combusts any fuel and produces steam or heats water or any other heat transfer medium [40 CFR §40.41c]] for which construction, modification, or reconstruction is commenced after June 9, 1989 and that have a maximum design heat input capacity of 100 million Btu per hour or less, but greater than or equal to 10 million Btu per hour.	И	The facility has no steam generating units with a maximum design heat input capacity of 100 MMBtu/hr or less, but greater than or equal to 10 MMBtu/hr. Therefore the facility is not subject to 40 CFR 60 subpart Dc.
Subpart GG Standards of Performance for Stationary Gas Turbines This rule applies to stationary gas turbines that commenced construction after October 3, 1977 and before February 18, 2005.	N	The facility has no stationary gas turbines. Therefore the facility is not subject to 40 CFR 60 subpart GG.
Subpart K Standards of Performance for Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced after June 11, 1973, and prior to May 19, 1978	r. N	The facility has no storage vessels for petroleum liquids for which construction, reconstruction, or modification occurred after June 11, 1973, and prior to May 19, 1978. Therefore the facility is not subject to 40 CFR 60 subpart K.
Subpart Ka Standards of Performance for Storage Vessels for Petroleum Liquids for which Construction, Reconstruction, or Modification Commenced after May 18, 1978, and prior to July 23, 1984	N	The facility has no storage vessels for petroleum liquids for which construction, reconstruction, or modification occurred after May 18, 1978, and prior to July 23, 1984. Therefore the facility is not subject to 40 CFR 60 subpart Ka.
Subpart Kb This rule applies to storage vessels with a capacity greater than or equal to 75 m3 [~471.7 bbl or ~19,813 gal] that are used to store Volatile Organic Liquids for which construction, reconstruction, or modification commenced after July 23, 1984.	N	The facility has no storage vessels for VOL that were constructed after July 23, 1984, with a capacity greater than or equal to 75 m3 (19,800 gal) or with a vapor pressure at or above 15 kPa. Therefore, the facility is not subject to 40 CFR 60 subpart Kb.
Subpart KKK Standards of Performance for Equipment Leaks of VOC from Onshore Natural Gas Processing Plants for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011  This rule applies to affected facilities in onshore natural gas processing plants (i.e., any processing site engaged in the extraction of natural gas liquids from field gas, fractionation of mixed natural gas liquids to natural gas products, or both [§60.631]).	N	The facility does not extract natural gas liquids from field gas or fractionate mixed natural gas liquids to natural gas products. Therefore, the facility is not subject to 40 CFR 60 subpart KKK.
Subpart LLL Standards of Performance for SO2 Emissions From On-Shore Natural Gas Processing for Which Construction, Reconstruction, or Modification Commenced After January 20, 1984, and on or Before August 23, 2011  This rule applies to affected facilities that process natural gas: each sweetening unit and each sweetening unit followed by a sulfur recovery unit.	N	The facility has no sweetening or sulfur recovery units. Therefore, the facility is not subject to 40 CFR part 60, subpart LLL.
Subpart IIII Standards of Performance for Stationary Compression Ignition Internal Combustion Engines  This rule applies to owner/operators of compression ignition (CI) internal combustion engines (ICE) that commence construction, modification, or reconstruction after July 11, 2005, where the stationary CI ICE are manufactured after April 1, 2006.	N	The facility has no compression ignition internal combustion engines. Therefore, the facility is not subject to 40 CFR 60, subpart IIII.
Subpart JJJJ Standards of Performance for Stationary Spark Ignition Internal Combustion Engines  This rule applies to owner/operators of spark ignition (SI) internal combustion engines (ICE) that commence construction after June 12, 2006, where the SI ICE is manufactured:  a. on or after July 1, 2007, for SI ICE with max rating ≥500 HP (except lean burn engines with max rating 500 ≤ HP < 1,350 HP;  b. on or after January 1, 2008 for lean burn engines with max rating 500 ≤ HP < 1,350 HP;  c. on or after July 1, 2008 for engines with max rating < 500 HP; or  d. on or after January 1, 2009 for emergency engines with a maximum engine power > 25 hp.	N	Units E1-E8 are >500 hp RICE that commenced construction prior to June 12, 2006 and were manufactured prior to July 1, 2007. Therefore, these units are not subject to 40 CFR Part 60, subpart JJJJ.
Subpart KKKK Standards of Performance for Stationary Combustion Turbines This rule applies to stationary combustion turbines and any associated heat recovery steam generator for units that commence construction, modification, or reconstruction after February 18, 2005.	N	The facility has no stationary combustion turbines. Therefore, the facility is not subject to 40 CFR 60 subpart KKKK.
Subpart OOO Standards of Performance for Crude Oil and Natural Gas Production, Transmission and Distribution for which Construction, Modification or Reconstruction Commenced after August 23, 2011, and on or before September 18, 2015  This rule establishes emission standards and compliance schedules for control of VOC and SO <sub>2</sub> emissions from affected facilities that commence construction, modification or reconstruction after August 23, 2011, and on or before September 18, 2015. Affected facilities include natural gas wells, centrifugal compressors, reciprocating compressors (unless located at a well site or an adjacent well site and servicing more than one well site), natural gas-driven continuous-bleed pneumatic devices, storage vessels, and onshore natural gas processing plants.	И	The facility is not a natural gas processing plant and does not include gas wells, storage vessels, continuous-bleed pneumatic devices, or compressors that have been constructed, modified, or reconstructed after August 23, 2011, and on or before September 18, 2015. Therefore, the facility is not subject to 40 CFR 60, subpart OOOO.
Subpart OOOa Standards of Performance for Crude Oil and Natural Gas Facilities for which Construction, Modification or Reconstruction Commenced after September 18, 2015  This rule establishes emission standards and compliance schedules for the control of the pollutant GHG, VOC, and SO2 emissions from affected facilities that commence construction, modification, or reconstruction after September 18, 2015.	N	The facility is not a natural gas processing plant and does not include gas wells, storage vessels, or continuous-bleed pneumatic devices that have been constructed, modified, or reconstructed after September 18, 2015.
Part 63 National Emission Standards for Hazardous Air Pollutants for Source Categories		Most of the standards set forth by these regulations do not apply to the facility because no applicable units exist at the facility. Specific standards which do not apply at the facility but may apply in general to natural gas production, transmission and/or processing facilities include:
Subpart A General Provisions  This rule applies to stationary sources containing an affected facility, the construction or modification of which is commenced after the date of publication in 40 CFR Part 63 of any standard applicable to the facility.	Y	As described in the following sections, the facility is subject to one or more standards of performance for new stationary sources. Therefore, the facility is subject to 40 CFR 60 subpart A.

## Applicability Determination

40 CFR Part	Description	Applicable Requirement	Reason
Subpart H	National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities  This rule applies to natural gas production facilities that process, upgrade, or store natural gas prior to the point at which the natural gas enters the natural gas transmission or storage source category or is delivered to the final end user. Affected sources include triethylene glycol (TEG) dehydration units located at area sources of HAP and; for major sources of HAP, each TEG dehydration unit and storage vessel (with a potential for flash emissions) and, for natural gas processing plants, the group of ancillary equipment, except compressors, intended to operate in volatile hazardous air pollutant service (as defined in §63.761).	Y	The facility is located prior to the point of custody transfer and is considered a production field facility under the subpart. The included GRI-GLYCalc 4.0 calculations demonstrate uncontrolled actual average benzene emissions from the TEG dehydration unit are less than 0.9 megagrams per year.  Therefore, per §63.764(e)(1)(ii), the TEG dehydration unit is exempt from the general standards for area sources at §63.764(d). However, recordkeeping requirements apply to the facility.
Subpart HH	IH National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities  This rule applies to natural gas transmission and storage facilities that are major sources of HAP emissions and that transport or store natural gas prior to entering the pipeline to a local distribution company or a final end user.	g N	The facility is not a natural gas transmission or storage facility. Therefore, the facility is not subject to 40 CFR 63, subpart HHH.
Subpart ZZZ	National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines  This rule establishes national emission limitations and operating limitations for HAP emitted from stationary reciprocating internal combustion engines (RICE).		Unit E1 is a non-emergency > 500 hp 4SRB SI RICE located at a major source of HAP and constructed after December 19, 2002. Therefore, this unit is subject to the requirements of 40 CFR part 63, subpart ZZZZ.
		Y	Units E2-E4 are non-emergency > 500 hp 4SLB SI RICE located at a major source of HAP and constructed prior to December 19, 2002. Therefore, these units are not subject to the requirements of 40 CFR part 63, subpart ZZZZ.
			Units E5-E8 are non-emergency > 500 hp 4SLB SI RICE located at a major source of HAP and constructed after December 19, 2002. Therefore, these units are subject to the requirements of 40 CFR part 63, subpart ZZZZ.
Subpart DDDI	National Emission Standards for Hazardous Air Pollutants for Major Sources: Industrial, Commercial, and Institutional Boilers and Process Heaters This rule applies to industrial, commercial and institutional boilers and process heaters that are located at a major source of HAP as defined in §63.2 or §63.761. TEG reboilers are not subject to this rule as they are listed as an affected source under subpart HH, per §63.7491(h).  Industrial boiler means a boiler used in manufacturing, processing, mining, and refining or any other industry to provide steam, hot water, and/or electricity.  Commercial/institutional boiler means a boiler used in commercial establishments or institutional establishments such as medical centers, research centers, institutions of higher education, hotels, and laundries to provide electricity, steam, and/or hot water.  Boiler means an enclosed device using controlled flame combustion and having the primary purpose of recovering thermal energy in the form of steam or hot water. Waste heat boilers are excluded from this definition.  Process heater means an enclosed device using controlled flame, that is not a boiler, and the unit's primary purpose is to transfer heat indirectly to a process material (liquid, gas, or solid) or to a heat transfer material for use in a process unit, instead of generating steam. Process heaters are devices in which the combustion gases do not directly come into contact with process materials. Process heaters do not include units used for comfort heat or space heat, food preparation for on-site consumption, or autoclaves.		The facility has no industrial, commercial, or institutional boilers as defined in this subpart. Therefore, the facility is not subject to 40 CFR 63, subpart DDDDD.
Subpart JJJJ	National Emission Standards for Hazardous Air Pollutants for Industrial, Commercial, and Institutional Boilers Area Sources  This rule applies to industrial, commercial, and institutional boilers that are located at area sources of HAP as defined in §63.2. TEG reboilers are not subject to this rule as they are listed as an affected source under subpart HH, per §63.11195(b).	N	The facility has no industrial, commercial, or institutional boilers as defined in this subpart. Therefore, the facility is not subject to 40 CFR 63, subpart JJJJJJ.
Part 64	Compliance Assurance Monitoring This rule applies to pollutant-specific emission units that are required to obtain a Part 70 permit if the unit satisfies the following criteria (per 40 CFR §64.2(a)(1-3) 1) Each unit that, by itself, has potential, pre-controlled emissions that are equal to or greater than the major source thresholds for an applicable regulated air pollutant and that is subject to an emission limitation or standard for the applicable regulated air pollutant; and 2) the unit uses a control device to achieve compliance with any such limitation or standard.	): N	The facility has no units with potential emissions equal to or greater than the major source thresholds for an applicable regulated air pollutant. Therefore, the facility is not subject to 40 CFR part 64.
Part 68	Chemical Accident Prevention Provisions  This rule applies to stationary sources that have more than a threshold quantity of a regulated substance in a process. Regulated substances include 77 toxic and 63 flammable substances, which are potentially present in the natural gas stream entering the facility and in the storage vessels located at the facility. The quantity of a regulated substance in a process is determined according to procedures presented under §68.115:  - §68.115(b)(1) and (2)(i) indicate that toxic and flammable substances in a mixture do not need to be considered when determining whether more than a threshold quantity is present at a stationary source if the concentration of the substance is below one percent by weight of the mixture.  - §68.115(b)(2)(iii) indicates that prior to entry into a natural gas processing plant, regulated substances in naturally occurring hydrocarbon mixtures need not be considered when determining whether more than a threshold quantity is present at a stationary source. Naturally occurring hydrocarbon mixtures include condensate, field gas, and produced water.  Condensate is defined under this subpart as the hydrocarbon liquid separated from natural gas that condenses because of changes in temperature, pressure, or both, and remains liquid at standard conditions.  Field gas is defined under this subpart as gas extracted from a production well before the gas enters a natural gas processing plant.  Produced water is defined under this subpart as water separated from natural gas after extraction.	a ld N	No substance listed by this regulations is stored at the facility in quantities above the applicable threshold values set forth by the regulation. Therefore, the facility is not subject to 40 CFR part 68.
Part 82	Protection of Stratospheric Ozone		Most of the standards set forth by these regulations do not apply to the facility because no applicable units or processes exist at the facility. Specific standards which do not apply at the facility but may apply in general to natural gas production, transmission and/or processing facilities include:
Subpart	F Recycling and Emissions Reduction The purpose of this rule is to reduce emissions of class I and class II refrigerants and their non-exempt substitutes to the lowest achievable level by maximizing the recapture and recycling of such refrigerants during the maintenance, service, repair and disposal of equipment containing the controlled substances.	N	There facility does not engage in any activities regulated under the subpart and has no equipment containing CFC's. Therefore, the requirements of 40 CFR part 82, subpart H are not applicable.

## Applicability Determination

40 CFR Part	Description	Applicable Requirement	Reason
Subpart	H Halon Emissions Reduction The purpose of this rule is to reduce emissions of halon by banning the intentional release of halons during repair, testing, and disposal of equipment containing halons.	N	There facility does not engage in any activities regulated under the subpart and has no equipment containing halon. Therefore, the requirements of 40 CFR part 82, subpart H are not applicable.
Part 98	Mandatory Greenhouse Gas Reporting This rule requires owners and operators of facilities that contain petroleum and natural gas and emit 25,000 metric tons or more of CO2e per year from process operations, stationary combustion, miscellaneous use of carbonates, and other source categories to report those emissions. Part 98 defines petroleum and natural gas facilities to which the 25,000 ton per year threshold applies as follows:  1) For the onshore petroleum and natural gas production industry segment, a facility is defined generally as all emission source types on a single well pad or associated with a single well pad and CO2 EOR operations that are under common ownership or control in a single hydrocarbon basin, as defined by the American Association of Petroleum Geologists. 2) For onshore natural gas processing industry segment, natural gas processing means the separation of natural gas liquids (NGLs) or non-methane gases from produced natural gas, or the separation of NGLs into one or more component mixtures. This segment also includes all residue gas compression equipment owned or operated by the natural gas processing plant. This industry segment includes processing plants that fractionate gas liquids, and processing plants that do not fractionate gas liquids but have an annual average throughput of 25 MMscf per day or greater. 3) For the onshore petroleum and natural gas gathering & boosting industry segment, a facility is defined generally as gathering pipelines and other equipment used to collect and/or treat petroleum and/or natural gas from onshore production wells for transport to a natural gas processing facility, a natural gas transmission pipeline or to a natural gas distribution pipeline. This segment covers sources that are not included in equipment reported under any other industry segment defined in this section. A gathering and boosting facility includes equipment and operations that are under common ownership or control in a single hydrocarbon basin, as defined by the American Association o	Y	The facility does emits 25,000 metric tons or more of CO <sub>2</sub> e per year. Therefore, the facility is subject to 40 CFR part 98.

#### Potential-to-Emit (PTE) Summary South Ignacio Central Delivery Point Red Cedar Gathering Company

Significant Emission Units			Emissions (tons/yr)									
Unit ID	Description	Rating	NO <sub>x</sub>	VOC	PM <sub>10</sub>	co	Total HAP	нсно	Benzene	CO2	Methane	CO₂e (MT/yr)
E1	Waukesha L7044GSI - Internal Combustion Engine (4SRB)	1,680 site-rated hp	40.3	5.8	1.1	56.5	1.8	1.2	0.0	6,359.8	13.3	6,692.2
E2	Waukesha L7042 GL - Internal Combustion Engine (4SLB)	1,337 site-rated hp	19.4	12.9	0.4	34.9	3.0	2.2	0.0	4,673.5	53.1	5,444.2
E3	Waukesha L7042 GL - Internal Combustion Engine (4SLB)	1,337 site-rated hp	19.4	12.9	0.4	34.9	3.0	2.2	0.0	4,673.5	53.1	5,444.2
E4	Waukesha L7042 GL - Internal Combustion Engine (4SLB)	1,337 site-rated hp	19.4	12.9	0.4	34.9	3.0	2.2	0.0	4,673.5	53.1	5,444.2
E5	Waukesha L5794LT - Internal Combustion Engine (4SLB)	1,401 site-rated hp	28.1	13.5	0.5	24.9	3.3	2.5	0.0	5,130.0	58.3	5,976.0
E6	Waukesha L5794LT - Internal Combustion Engine (4SLB)	1,401 site-rated hp	28.1	13.5	0.5	24.9	3.3	2.5	0.0	5,130.0	58.3	5,976.0
E7	Waukesha L5794LT - Internal Combustion Engine (4SLB)	1,401 site-rated hp	28.1	13.5	0.5	24.9	3.3	2.5	0.0	5,130.0	58.3	5,976.0
E8	Waukesha L5794LT - Internal Combustion Engine (4SLB)	1,401 site-rated hp	28.1	13.5	0.5	24.9	3.3	2.5	0.0	5,130.0	58.3	5,976.0
	Subtotal Sig	nificant Emission Units	210.9	98.7	4.3	260.6	24.4	17.8	0.2	40,900.2	405.8	46,928.6

Insignificant	Emission Units (IEU)						Emission	s (tons/yr	)			
Unit ID	Description	Rating	NO <sub>x</sub>	VOC	PM <sub>10</sub>	co	Total HAP	нсно	Benzene	CO2	Methane	CO₂e (MT/yr)
D1	TEG Dehydrator	30 MMscfd	0.0	1.2	0.0	0.0	0.3	0.0	0.3	40.9	3.7	120.3
D2	TEG Dehydrator	40 MMscfd	0.0	1.1	0.0	0.0	0.4	0.0	0.4	19.1	17.6	415.9
TK-501	Used oil storage tank	500 bbl	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-502	Used oil storage tank	500 bbl	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-503	Dehy still vent drain tank	95 bbl	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-504	Lubricating oil storage tank (E1)	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-505	Lubricating oil storage tank (E2)	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-506	Lubricating oil storage tank (E3)	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-507	Lubricating oil storage tank (E4)	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-508	Lubricating oil storage tank (E5)	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-509	Lubricating oil storage tank (E6)	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-510	Lubricating oil storage tank (E7)	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-511	Lubricating oil storage tank (E8)	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-512	Used oil storage tank (E1)	250 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-513	Used oil storage tank (E2)	250 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-514	Used oil storage tank (E3)	250 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-515	Used oil storage tank (E4)	250 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-516	Used oil storage tank (E5)	250 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-517	Used oil storage tank (E6)	250 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-518	Used oil storage tank (E7)	250 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-519	Used oil storage tank (E8)	250 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-520	Ethylene glycol storage tank	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-521	TEG storage tank	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
TK-522	TEG storage tank	500 gal	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
RB1	TEG dehydrator reboiler heater (D1)	1.750 MMBtu/hr	0.9	0.0	0.1	0.7	0.1	0.0	0.0	1,022.0	0.0	927.6
RB2	TEG dehydrator reboiler heater (D2)	0.750 MMBtu/hr	0.4	0.0	0.0	0.3	0.0	0.0	0.0	438.0	0.0	397.5
H-101	Used oil storage tank heater (TK-501)	0.325 MMBtu/hr	0.2	0.0	0.0	0.1	0.0	0.0	0.0	189.8	0.0	172.3
H-102	Used oil storage tank heater (TK-502)	0.325 MMBtu/hr	0.2	0.0	0.0	0.1	0.0	0.0	0.0	189.8	0.0	172.3
H-103	Catalytic heater	0.008 MMBtu/hr	0.0	0.0	0.0	0.0	0.0	0.0	0.0	4.7	0.0	4.2
FUG	Fugitive Emissions		0.0	0.1	0.0	0.0	0.0	0.0	0.0	10.2	207.0	5,186.3
******************************	Subtotal Insig	gnificant Emission Units	1.5	2.5	0.1	1.3	0.9	0.0	0.7	1,914.4	228.3	7,396.5
************************************		Total	212.5	101.2	4.4	261.9	25.3	17.8	0.9	42,814.6	634.1	54,325.1

## Waukesha L7044GSI Emission Calculations South Ignacio Central Delivery Point Red Cedar Gathering Company

### Waukesha L7044GSI - Internal Combustion Engine (4SRB)

Unit F1

Manufacturer Unit Rating:	1,680 hp @ 1,200 rpm
Site Specific Unit Rating <sup>a</sup> :	1,680 hp @ 6,320 ft
BSFC:	7,881 btu/hp-hr
Maximum Heat Input:	13.2 MMBtu/hr
Operating Schedule:	8,760 hr/yr
Maximum Fuel Use <sup>b</sup> :	128.5 mmscf/yr

<sup>&</sup>lt;sup>a</sup> Based on manufacturer's site derate of 2% for every 1,000 ft above 8,000 ft elevation.

#### Potential Criteria Pollutant Emissions

	Uncontrolled Emissions								
Pollutant	Emission Factors	Data Source	(lb/hr)	(ton/yr)					
NO <sub>X</sub>	13.30 g/hp-hr	Engine Manufacturer	49.26	215.76					
CO	11.20 g/hp-hr	Engine Manufacturer	41.48	181.69					
voc	0.36 g/hp-hr	Engine Manufacturer	1.33	5.84					
PM <sub>10</sub>	1.94E-02 lb/MMBtu	AP-42, Table 3.2-3	0.26	1.12					
SO <sub>2</sub>	5.88E-04 lb/MMBtu	AP-42; Table 3.2-3	0.01	0.03					
CO <sub>2</sub>	110.0 lb/MMBtu	AP-42; Table 3.2-3	1,452.00	6,359.76					
Methane	0.23 lb/MMBtu	AP-42; Table 3.2-3	3.04	13.30					
CO <sub>2</sub> e				6,692.2 MT/yr					

Federally Enforceable Emissions

		Controlled	Emissions	
Pollutant	Emission Factors	Data Source	(lb/hr)	(ton/yr)
$NO_X$	2.48 g/hp-hr	Calculated (based on	9.20	40.30
CO	3.48 g/hp-hr	SMNSR lb/hr limits)	12.90	56.50

Hazardous Air Pollutant (HAP) Emissions

			Uncontrolle	d Emissions
Pollutant	Emission Factors <sup>c</sup>	Data Source	(lb/hr)	(ton/yr)
1,3-Butadiene	6.63E-04 lb/MMBtu	AP-42; Table 3.2-3	8.75E-03	3.83E-02
Acetaldehyde	2.79E-03 lb/MMBtu	AP-42; Table 3.2-3	3.68E-02	0.16
Acrolein	2.63E-03 lb/MMBtu	AP-42; Table 3.2-3	3.47E-02	0.15
Benzene	1.58E-03 lb/MMBtu	AP-42; Table 3.2-3	2.09E-02	9.13E-02
Formaldehyde	2.05E-02 lb/MMBtu	AP-42; Table 3.2-3	2.71E-01	1.19
Methanol	3.06E-03 lb/MMBtu	AP-42; Table 3.2-3	4.04E-02	0.18
Toluene	5.58E-04 lb/MMBtu	AP-42; Table 3.2-3	7.37E-03	3.23E-02
Xylene	1.95E-04 lb/MMBtu	AP-42; Table 3.2-3	2.57E-03	1.13E-02
Total	***		< 0.42	< 1.85

<sup>&</sup>lt;sup>c</sup> Uncontrolled emission factors for 4-stroke, rich-burn (4SRB) engines based on the highest emission factor between EPA's AP-42, GRI field data and GRI literature data sets, and the manufacturer's data.

<sup>&</sup>lt;sup>b</sup> Based on LHV of: 900 btu/scf

#### STANDARD EQUIPMENT

AIR CLEANER - Two, dry type with rain shield and service indicator.

BARRING DEVICE - Manual

**BEARINGS** - Heavy duty, replaceable, precision type.

**BREATHER** - Closed system.

CONNECTING RODS - Drop forged steel, rifle drilled.

CONTROL SYSTEM - Pneumatic. Includes pilot operated valves for air start and prelube. Engine mounted control panel with two push button valves. Pilot operated air start valves omitted when starter is not furnished by Waukesha. Includes engine On/Off push button. One mounted on either side of the engine.

CRANKCASE - Integral crankcase and cylinder frame. Main bearing caps drilled and tapped for temperature sensors. Does not include sensors.

CRANKSHAFT - Forged steel, seven main bearings, counterweighted and dynamically balanced.

CYLINDERS - Removable wet type cylinder liners, chrome plated on outer diameter.

CYLINDER HEADS - Twelve interchangeable. Four valves per cylinder, with water cooled exhaust valve seats. Roller valve lifters and hydraulic push rods. Flange mounted ignition coils.

ENGINE MONITOR DEVICES - Thermocouples, K-type, are wired to a bulk head connector for jacket water temperature, tube oil temperature and intake manifold temperature. 25 foot (7.6 m) customer interface and standard thermocouple harnesses are provided for making connections to a customer supplied panel. Magnetic pickup wired for customer supplied tachometer. Lube oil pressure and intake manifold pressure sensing lines are terminated in a common bulk head.

ENGINE ROTATION - Counterclockwise when facing flywheel.

FLYWHEEL - Approx. WR2 = 155000 lb-in2, with ring gear (208 teeth), machined to accept two drive adapters: 31 88" (810 mm) pilot bore, 30.25" (768 mm) bolt circle, (12) 0.75" 10 tapped holes; or 28.88" (734 mm) pilot bore, 27.25" (692 mm) bolt circle, (12) 0.625"-11 tapped holes and (12) 0.75"-10 tapped holes.

FLYWHEEL HOUSING - No. 00 SAE.

FUEL SYSTEM - Two natural gas, 4" (102 mm) updraft carburetors and two Fisher Model 99, 2" (51 mm) gas regulators, mounted, 25 psi (172 kPa) fuel inlet pressure required.

GOVERNOR - Woodward UG-8 LD hydraulic lever type, with friction type speed control. Mounted on right hand side.

IGNITION SYSTEM - Waukesha Custom Engine Control Ignition Module. Electronic digital ignition system. 24V DC power required.

INTERCOOLER - Air-to-water.

LEVELING BOLTS

LIFTING EYES - Requires 9.5 ton Working Load Limit (W.L.L.) anchor shackles.

LUBRICATION - Full pressure, gear type pump. Full flow lube oil filter with replaceable depth-type elements and flexible connections, shipped loose. MICROSPIN® bypass filter, engine mounted. Lube oil strainer, mounted. Air/gas motor driven prelube pump, requires final piping.

MANIFOLDS - Exhaust, (2) water cooled.

OIL COOLER - Shell and tube type, with thermostatic temperature controller and pressure regulating valve. Factory mounted.

OIL PAN - Base type. 90 gallon (340 L) capacity, including filter and cooler.

PAINT - Oilfield orange primer.

PISTONS - Aluminum with floating pin. Oil cooled. 8:1 compression ratio

SHIPPING SKID - Steel for domestic truck or rail.

TURBOCHARGERS - (2) with water-cooled bearing housing and adjustable wastegates. Single vertical exhaust outlet at rear. Flexible stainless steel exhaust connection with 8" (203 mm) pipe flange.

VIBRATION DAMPER - Viscous type.

#### WATER CIRCULATING SYSTEM

Auxiliary Circuit - Belt driven water circulating pump for intercooler and tube oil cooler.

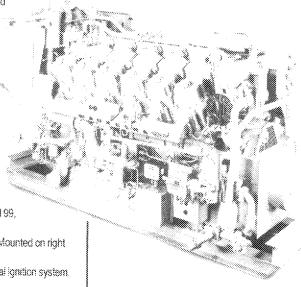
Engine Jacket - Belt driven water circulating pump. Cluster type thermostatic temperature regulating valve, full flow bypass type with 165° - 170° F (74° - 77° C) start to open thermostatis. Flange connections and mating flanges for (2) 4" (102 mm) inlets and (1) 5" (127 mm) outlet.

WAUKESHA CUSTOM ENGINE CONTROL, DETONATION SENSING MODULE (DSM) — includes individual cylinder sensors, Detonation Sensing Module, filter and cables. Compatible with Waukesha CEC Ignition Module only. Detonation Sensing Module and filter are mounted and wired. Packager is responsible for 24V DC power supply and ground to the DSM. The DSM meets Canadian Standards Association Class I, Division 2, Group D hazardous location requirements.



# L7044GS

**VHP™ Series Four** 1120 - 1680 BHP



Model L7044GSI Turbocharged and intercooled, Twelve Cylinder, Four-Cycle Gas Engine

## SPEOPLO ATIONS

) ISO 900

#### CONTINUOUS POWER RATINGS: L7044GSI VHP SERIES FOUR

				srake Hors	epower (k		
Model	I.C. Water Inlet Temp. °F (°C) (Tora)	CR.	800 rpm	900 rpm	1000 rpm	1100 rpm	1286 rpm
L7044GSI	130° (54°)	8:1	1120 (836)	1250 (940)	1400 (1044)	1540 (1149)	1680 (1263)

Rating Standard: All models: Ratings are based on ISO 3046/1-1995 with mechanical efficiency of 90% and auxiliary water temperature Tora (clause 10.1) as specified above limited to ± 10° F (± 5° C). Ratings are also valid for SAE J1349, BS5514, DIN6271 and AP17B-11C standard atmospheric conditions.

ISO Standard Power/Continuous Power Rating: The highest load and speed which can be applied 24 hours a day, seven days a week, 365 days per year except for normal maintenance, it is permissible to operate the engine at up to 10% overload, or maximum load indicated by the intermittent rating, whichever is lower, for two hours in each 24 hour period.

All natural gas engine ratings are based on a fuel of 900 Blu/ft\* (35.3 MJ/nm²) SLHV value, with a 91 Waukesha Knock Index®.

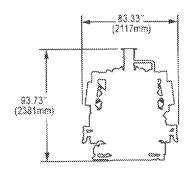
For conditions or fuels other than standard, the Waukesha Engine Sales Engineering Department.

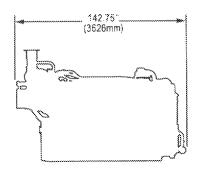
#### PERFORMANCE: 1.7044GSI VHP SERIES FOUR

English 1901 F	English 130° F LC. Water Temperature		Metric 54° C I.C. Water Temperature		
RPM	1200 1000	RPM	1200 1000		
Power (Bhp)	1680 1400	Power (kWb)	1253 1044		
BSFC (Blu/bhp-hr)	7780 7685	BSFC (kJ/kW-br)	11009 10874		
NOx (grams/bhp-hr)	126 121	NOx (g/nm²)	47 45		
CO (grams/bhp-hr)	138 122	CO (g/nim²)	5.1 4.5		
NMHC (grams/bhphr)	036 036	NMHC (g/nm²)	0.13 0.13		
BSFC (Btu/bhp-hr)	7595 7535	BSFC (g/nm³)	10747 10662		
NOx (grams/bhp-hr)	21.3 (20.7	NOx (g/nm²)	79:77		
CO (grams/bhp-hr)	- 6	CO (g/nm²)	06 06		
NMHC (grams/bhp-hr)	0.30 0.30	NMHC (g/nm²)	0.11 0.11		

#### NOTES:

- Fuel consumption and exhaust emissions are based on ISO 3046/1-1295 standard reference conditions and commercial quality natural gas of 900 Bhu/ft<sup>3</sup>
  (35.38 ML/m<sup>3</sup> [25, V(0; 101.325)]) saturated lower heat value. Waukesha Knock Index\* of 91 and 93% methane content by volume. ISO 3046/1-1995 standard reference conditions are 77°F (25°C) ambient temperature, 29.54 inches Hg (100 kPa) barometric pressure, 30% relative humidity (1kPa/0.3 inches Hg water vapor pressure).
- 2) S.I. exhaust emissions are corrected to 5% O, (0°C and 101.325 kPa).
- 3) Data will vary due to variations in site conditions. For conditions and/or fuels other than standard, consult the Waukesha Engine Sales Engineering Department.







WAUKESHA ENGINE DRESSER, INC. 1000 West St. Paul Avenue Waukesha, WI 53188-4999 Phone: (262) 547-3311 Fax: (252) 549-2795 Waukeshaengine.dresser.com

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WAUKESHA ENGINE DRESSER INDUSTRIAL PRODUCTS, B.V. Farmsumerweg 43, Postbus 330 9900 AH Appingedam, The Netherlands Phone: (31) 598-852222 Fax: (31) 598-828111 Consuit your local Waukesha Distributor for system application assistance. The manufacturer reserves the right to change or modify without notice, the design or equipment specifications as herein set forth without incurring any obligation either with respect to equipment previously sold or in the process of construction except where otherwise specifically guaranteed by the manufacturer.

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# Adjustments To Engine And Enginator Systems For High Altitude And High Temperature<sup>12, 15</sup> For Natural Gas, Low BTU and HD-5 Propane Fuels Continued

		Turbocharged and Intercooled	Continuous/ Prime Power*	Intermittent/ Standby
VHP F3521/L5790	Altitude:	Deduct 2% for each 1000 ft. (305 m) above;	6000 ft. 1828 m	1500 ft. 457 m
L7042/P9390GSI	Temperature <sup>17</sup> :	Deduct 1% for each 10°F (5.5°C) above;	100°F 38°C	100°F 38°C
VHP F3514/F3524/L5794/L7044GSI <sup>13</sup>	Altitude:	Deduct 2% for each 1000 ft (305 m) above:	<b>8000 ft</b> . 2436 m	<b>4000 ft</b> 1219 m
	Temperature <sup>17</sup> :	Deduct 1% for each 10°F (5.5°C) above:	100°F 38°C	<b>100°F</b> 38°C
VHP GL	Altitude:	Deduct 2% for each 1000 ft. (308 m) above:	1500 ft. 457 m	1500 ft - 457 m
	Temperature <sup>u</sup> :	Deduct 1% for each 10°F (5.5°C) above:	100°F 38°C	85°F - 29°C
VHP L5774LT*	Altitude: Temperature <sup>i7</sup> :	Deduct 2.4% for each 1000 ft. (306 m) above: Deduct 2.4% for each 10°F (5.5°C) above:	5000 ft. 1524 m 100°F 38°C	<u> </u>
VHP L5794LT	Altitude:	Deduct 2.4% for each 1000 ft. (306 m) above:	<b>5000 ft</b> . 1524 m	1500 ft   457 m
	Temperature <sup>17</sup> :	Deduct 2.4% for each 10°F (5.5°C) above:	100°F 38°C	85°F   29°C
VHP F3521/L5790/L7042GL with	Altitude:	Deduct 2% for each 1000 ft. (305 m) above:	1500 ft. 457 m	1500 ft   457 m
Low Fuel Pressure System Option	Temperature¹':	Deduct 4% for each 10°F (5.5°C) above:	100°F 38°C	85°F   29°C
VHP F3521/L5790/L7042GSI with	Altitude:	Deduct 2% for each 1000 ft. (308 m) above:	3000 ft. 914 m	<b>1500 ft</b> 457 m
Low Fuel Pressure System Option	Temperature <sup>17</sup> :	Deduct 4% for each 10°F (5.6°C) above:	100°F 38°C	<b>85°F</b> 29°C
VHP F3524/L5794/L7044GSI with	Altitude:	Deduct 2% for each 1000 ft. (305 m) above:	3000 ft. 914 m	1500 ft -457 m
Low Fuel Pressure System Option	Temperature¹':	Deduct 4% for each 10°F (3.5°C) above:	100°F 38°C	85°F 29°C
VHP L5794LT with Low Fuel	Altitude:	Deduct 4.8% for each 1000 ft. (⋘ m) above:	1500 ft. 457 m	1500 ft -457 m
Pressure System Option	Temperature <sup>17</sup> :	Deduct 4.8% for each 10°F (≾.5°C) above:	100°F 38°C	85°F -29°C
VHP GSI and GL HD-5/Propene (Including 3524/5794/7044GSI**)	Altitude: Altitude: Altitude: Temperature <sup>17</sup> : Jacket Water Temp.:	Deduct 2% for each 1000 ft. (308 m) above (GL only); Deduct 2% for each 1000 ft. (308 m) above (GSt only); Deduct 2% for each 1000 ft. (308 m) above (Series Four GSt only); Deduct 1% for each 10°F (5.5°C) above; Deduct 2.5% for each 10°F (6.5°C) above;	1500 ft. 487 m 6000 ft. 1828 m 8000 ft. 2438 m 100°F 38°C 180°F 82°C	
APG 16V150LTD	Altitude: Temperature <sup>17</sup> :	Contact Waukesha Application Engineering above: Contact Waukesha Application Engineering above:	1500 ft. 457 m 100°F 38°C	
APG 12V220GL APG 18V220GL	Altitude: Temperature <sup>i</sup> ':	Contact Waukesha Application Engineering Contact Waukesha Application Engineering	·····	
8L-AT27GL	Altitude:	Deduct 3.3% for each 1000 ft. (365 m) above:	3000 ft. 914 m	800 ft. 244 m
12V-AT27GL 16V-AT27GL GC	Temperature <sup>17</sup> : Altitude: Temperature <sup>17</sup> :	Deduct 2% for each 10°F (5.5°C) above:  Deduct 4% for each 1000 ft. (305 in) above:  Deduct 2% for each 10°F (5.5°C) above:	100°F 38°C 6000 ft. 1828 m 100°F 38°C	100°F 38°C 6000 ft. 1828 m 100°F 38°C
16V-AT27GL EPG	Altitude:	Contact Waukesha Application Engineering above:	1000 ft. 365 m	800 ft. 244 m
	Temperature <sup>17</sup> :	Contact Waukesha Application Engineering above:	100°F 38°C	100°F 38°C
		Naturally Aspirated		
All VHP, VGF and VSG	Altitude:	Deduct 3% for each 1000 ft. (305 m) above:	1500 ft. 457 m	<b>500 ft.</b> 152 m
Natural Gas	Temperature <sup>17</sup> :	Deduct 1% for each 10°F (5.5°C) above:	100°F 38°C	<b>85°F</b> 29°C
All VHP, VGF, VSG HD-5/Propane	Altitude: Temperature <sup>r</sup> : Jacket Water Temp.:	Deduct 3% for each 1000 ft. (305 m) above: Deduct 5.5% for each 10°F (5.5°C) above: Deduct 2.5% for each 10°F (5.5°C) above:	1500 ft 457 m 100°F 38°C 180°F 32°C	

#### NOTES:

Rating Standard: All models: Ratings conform to ISO 3046/1 (latest version) with a mechanical efficiency of 90% and auxiliary water temperature, Tora, as specified in the Power Rating Chart, Bulletin 1079 (latest version) limited to ±10° F (±5.5° C). Ratings are also valid for SAE J1349, BS 5514, DIN 6271 and API 7B-11C standard atmospheric reference conditions.

Fuel Standard: All natural gas engine ratings are based on 900 BTU/ft² (35.38 MJ/m² [25, V(0; 101.325)]) SLHV, 91 WKI™ minimum, commercial quality natural gas. Refer to S-7884-7 (latest version) for full gaseous fuel specifications.

ISO Standard Power (Continuous Power Rating): The highest load and speed that can be applied 24 hours per day, seven days per week, 365 days per year except for normal maintenance at ISO standard ambient reference conditions, it is permissible to operate the engine at up to 110% of the ISO Standard Power or the maximum power indicated by the intermittent rating, whichever is lower, for two hours in every 24 hour period.

ISO Service Power (Site Continuous Power Rating): The highest load and speed that can be applied 24 hours per day, seven days per week, 366 days per year except for normal maintenance at the operating and ambient conditions of the site application. Unless otherwise stated, it is permissible to operate the engine at up to 110% of the ISO Service Power (see the Overload Power definition) or the intermittent power rating available at the site operating and ambient conditions, whichever is lower, for two hours in every 24 hour period.

Overload Power: The power that an engine is permitted to supply, with a duration and frequency of use depending upon the service application, at stated ambient conditions, immediately after operating at its ISO Service Power rating. Unless otherwise stated, it is permissible to operate the engine at up to 110% of the ISO Service Power or the intermittent power rating available at the site operating and ambient conditions, whichever is lower, for two hours in every 24 hour period. For situations without a defined intermittent power, the allowable 10% overload power is reduced from ISO standard ambient reference conditions by the applicable rating adjustments listed in the Intermittent/Standby Power column.

Intermittent Power Rating: The highest load and speed that can be applied in variable speed mechanical system applications only. Operation at this rating is limited to a maximum of 3500 hours per year.

Generator Continuous Power Rating (kWe): The highest load and speed which can be applied 24 hours per day, seven days per week, 365 days per year except for normal maintenance. Unless otherwise stated, it is permissible to operate the engine at up to 110% of the generator continuous power rating for two hours in every 24 hour period.

Generator Standby Power Rating (kWe): This rating applies to those systems used as a secondary source of electrical power. This rating is the output the system will produce continuously 24 hours per day for the duration of the prime power source outage. No overload is allowed. This rating may reduce the lifecycle intervals.

Generator Peak Shaving Application Rating (kWe) For VHP Models Only: This rating is based on the number of horsepower-hours available per year in a constant speed application at site conditions. This rating allows for limited engine operation above the published ISO Standard Power rating for VHP models only. This rating class requires a Special Application Approval. Contact Waukesha's Sales Engineering Department. This rating may reduce the lifecycle intervals.

- 12 These altitude and temperature adjustments are meant to be a guide only and cannot be applied without limit. Contact Waukesha's Sales Engineering Department for additional information.
- 13 The F3514GSI/F3524GSI, L5794GSI, and L7044GSI models are limited to 180°F maximum jacket water temperature.
- 14 The L5774LT is rated for 130°F intercooler water temperature only.
- 15 Unless otherwise specified, overload power is available for two hours in every 24 hour period at a level specified in the Notes section (above) or on a Special Application Approval.
- 16 For complete information regarding operation on propane and other fuels, including proper ignition timing, see the most current, model specific S-07079 series Technical Data Sheets.
- 17 Temperature is defined as the engine combustion air inlet temperature.
- 18 Gas compression application only. Applies to 160 BMEP rating.
- \*For Peak Shaving derates, contact the Waukesha Sales Engineering Department.

## Waukesha L7042GL Emission Calculations South Ignacio Central Delivery Point Red Cedar Gathering Company

### Waukesha L7042 GL - Internal Combustion Engine (4SLB)

Units E2 - E4

Manufacturer Unit Rating:	1,480 hp @ 1,200 rpm
Site Specific Unit Rating <sup>a</sup> :	1,337 hp @ 6,320 ft
BSFC:	7,284 btu/hp-hr
Maximum Heat Input:	9.7 MMBtu/hr
Operating Schedule:	8,760 hr/yr
Maximum Fuel Use <sup>b</sup> :	94.4 mmscf/yr

<sup>&</sup>lt;sup>a</sup> Based on manufacturer's site derate of 2% for every 1,000 ft above 1,500 ft elevation.

#### Potential Criteria Pollutant Emissions

Pollutant		Uncontrolled Emissions			
	Emission Factors	Data Source	(lb/hr)	(ton/yr)	
NO <sub>X</sub>	1.50 g/hp-hr	Engine Manufacturer	4.42	19.37	
co	2.70 g/hp-hr	Engine Manufacturer	7.96	34.86	
VOC	1.00 g/hp-hr	Engine Manufacturer	2.95	12.91	
PM <sub>10</sub>	9.99E-03 lb/MMBtu	AP-42; Table 3.2-2	0.10	0.42	
SO <sub>2</sub>	5.88E-04 lb/MMBtu	AP-42; Table 3.2-2	0.01	0.02	
CO <sub>2</sub>	110.00 lb/MMBtu	AP-42; Table 3.2-2	1,067.00	4,673.46	
Methane	1.25 lb/MMBtu	AP-42; Table 3.2-2	12.13	53.11	
CO <sub>2</sub> e				5,444.15 MT/yr	

Hazardous Air Pollutant (HAP) Emissions

Pollutant	Emission Factors <sup>c</sup>	Data Source	Uncontrolled Emissions	
			(lb/hr)	(ton/yr)
1,3-Butadiene	2.67E-04 lb/MMBtu	AP-42; Table 3.2-2	2.59E-03	1.13E-02
2,2,4-Trimethylpentane	2.50E-04 lb/MMBtu	AP-42; Table 3.2-2	2.43E-03	1.06E-02
Acetaldehyde	8.36E-03 lb/MMBtu	AP-42; Table 3.2-2	8.11E-02	0.36
Acrolein	5.14E-03 lb/MMBtu	AP-42; Table 3.2-2	4.99E-02	0.22
Benzene	4.40E-04 lb/MMBtu	AP-42; Table 3.2-2	4.27E-03	1.87E-02
Biphenyl	2.12E-04 lb/MMBtu	AP-42; Table 3.2-2	2.06E-03	9.01E-03
Formaldehyde	5.28E-02 lb/MMBtu	AP-42; Table 3.2-2	5.12E-01	2.24
Methanol	2.50E-03 lb/MMBtu	AP-42; Table 3.2-2	2.43E-02	0.11
n-Hexane	1.11E-03 lb/MMBtu	AP-42; Table 3.2-2	1.08E-02	4.72E-02
Toluene	4.08E-04 lb/MMBtu	AP-42; Table 3.2-2	3.96E-03	1.73E-02
Xylene	1.84E-04 lb/MMBtu	AP-42; Table 3.2-2	1.78E-03	7.82E-03
Total			< 0.70	< 3.05

c Uncontrolled emission factors for 4-stroke, lean-burn (4SLB) engines based on the highest emission factor between EPA's AP-42, GRI field data and GRI literature data sets, and the manufacturer's data.

<sup>&</sup>lt;sup>b</sup> Based on LHV of 900 btu/sc

## STANDARD EQUIPMENT

AIR CLEANER - Two, dry type with rain shield and service indicator.

BARRING DEVICE - Manual.

BEARINGS - Heavy duty, replaceable, precision type

BREATHER - Closed system.

CONNECTING RODS - Drop forged steel, rifle drilled.

CONTROL SYSTEM – Pneumatic. Includes pilot operated valves for air start and prelube. Engine mounted control panel with two push button valves. Pilot operated air start valves omitted when starter is not furnished by Waukesha. Includes engine On/Off push button. One mounted on either side of the engine.

CRANKCASE – Integral crankcase and cylinder frame. Main bearing cape drilled and tapped for temperature sensors. Does not include sensors.

CRANKSHAFT - Counterweighted, forged steel, seven main bearings, and dynamically balanced.

CYLINDERS - Removable wet type cylinder liners, chrome plated on outer diameter, induction hardened.

CYLINDER HEADS – Twelive interchangeable. Two hard faced intake and two hard faced exhaust valves per cylinder. Hard faced intake and exhaust valve seat inserts. Roller valve lifters and hydraulic push rods. Includes prechamber and related fuel control valves.

ENGINE ROTATION - Counterclockwise when facing flywheel.

ENGINE MONITORING DEVICES - Engine thermocouples, K-type, for jacket water temperature, lube oil temperature, intake manifold temperature, individual cylinder exhaust temperature and a common pre turbine temperatures, one on each bank. Magnetic pickup wired for customer supplied tachometer. Lube oil pressure and intake manifold pressure sensing lines are terminated in a common bulk head.

EXHAUST OUTLET - Single vertical at rear. Flexible stainless steel connection with 8" (203 mm) pipe flange.

FLYWHEEL - Approx. WR? = 155000 lb-in\*; with ring gear (208 teeth), machined to accept two drive adapters: 31.88" (810 mm) pilot bore, 30.25" (768 mm) bolt circle, (12) 0.75"-10 tapped holes; or 28.88" (734 mm) pilot bore, 27.25" (692 mm) bolt circle, (12) 0.825"-11 tapped holes and (12) 0.75"-10 tapped holes.

FLYWHEEL HOUSING - No. 00 SAE.

FUEL SYSTEM - Dual natural gas, 4" (102 mm) duplex updraft carburetors. Two Fisher Model 99, 2" (51 mm) gas regulators.

30 - 50 psi (241 - 345 kPa) gas inlet pressure required. Prechamber fuel system and control logic.

GOVERNOR - Woodward UG-8 LD hydraulic lever type, with friction type speed control. Mounted on right hand side.

IGNITION – Waukesha Custom Engine Control Ignition Module, Electronic digital ignition system, 24V DC power required.

INTERCOOLER - Air-to-water.

LEVELING BOLTS

LIFTING EYES

LUBRICATION – Full pressure. Gear type pump, Full flow filter, 36 gallon (136 litres) capacity, not mounted, includes flexible connections, includes lube oil strainer, mounted on engine. Air/gas motor driven prelube pump. Requires final piping.

MANIFOLDS - Exhaust, (2) water cooled.

OIL COOLER - With thermostatic temperature controller and pressure regulating valve. Not mounted.

OIL PAN - Base type, 90 gallon (340 litres) capacity including filter and cooler.

PAINT - Oiffield orange primer.

PISTONS - Aluminum with floating pin. 10.5:1 compression ratio. Oil cooled.

SHIPPING SKID - Steel for domestic truck or rail

TURBOCHARGERS - Two, dry type. Wastegate controlled.

VIBRATION DAMPER - Two, viscous type. Guard included with remote mounted radiator or no radiator. WATER CIRCULATING SYSTEM

Auxiliary Circuit - For oil cooler and intercooler. Pump is belt driven from crankshaft pulley, includes thermostatic valve.

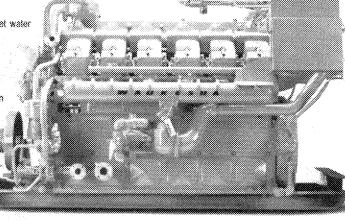
Engine Jacket – Beit driven water circulating pump, cluster type thermostatic temperature regulating valve, full flow bypass type. Flange connections and mating flanges for (2) 4" (102 mm) inlets and (1) 5" (127 mm) outlet.

WAUKESHA CUSTOM ENGINE CONTROL, DETONATION SENSING MODULE (DSM) — includes individual cylinder sensors, Detonation Sensing Module, filter and cables. Device is compatible with Waukesha CEC Ignition Module only. Sensors are mounted and wired to engine junction box. Detonation Sensing Module and filter are shipped loose. One 11 ft. cable provided for connection between engine junction box and filter. One each 15 ft. cable provided for connection between filter and DSM and Ignition Module and DSM. One 20 ft. cable provided for power and ground for filter. All cables are shipped loose. Packager is responsible for power supply and ground to the DSM. 24V DC power is required. The DSM meets Canadian Standards Association Class 1, Group D. Division 2, hazardous location requirements.



# L7042GL

VHP<sup>™</sup> Series Gas Engine 886 - 1547 BHP



Model L7042GL Turbocharged and Intercooled, Twelve Cylinder, Lean Combustion, Four-Cycle Gas Engine

## SPECIFICATIONS

Professional

Enlessens No. 10 objects 10 objects 10 objects

## POWER RATINGS: L7042GL VHP SERIES GAS ENGINES

	100000				sepower (k	wer (kWb Output)		
Model	I.C. Water In		C.R.	800 rpm	900 rpm	1000 rpm	1100 rpm	1200 rpm
High Speed Turbo'	85° (2	9°)	10.5:1	928 (892)	1160 (865)	1289 (961)	1418 (1057)	1547 (1154)
High Speed Turbo <sup>1</sup>	130° (5		10.5:1	886 (661)	1108 (826)	1232 (919)	1355 (1010)	1478 (1102)
Low Speed Turbo	85° (2		10.5.1	1031 (769)	1160 (865)	1289 (961)		
Low Speed Turbo <sup>2</sup>	130° (5		10.5:1	985 (735)	1108 (826)	1232 (919)		

"High speed turbocharger match – 1001-1200 rpm "Low speed turbocharger match – 700-1000 rpm

Rating Standard: All models: Ratings are based on ISO 3046/1-1995 with mechanical efficiency of 90% and auxiliary water temperature Tora (clause 10.1) as specified above limited to ± 10° F (± 5° C). Ratings are also valid for SAE J1349, BS5514, DIN6271 and AP178-11C standard atmospheric conditions.

ISO Standard Power/Continuous Power Rating: The highest load and speed which can be applied 24 hours a day, seven days a week, 365 days per year except for normal maintenance. It is permissible to operate the engine at up to 10% overload, or maximum load indicated by the intermittent rating, whichever is lower, for two hours in each 24 hour period.

All natural gas engine ratings are based on a fuel of 900 Bhu/ft<sup>3</sup> (36.3 MJ/mm<sup>2</sup>) SLHV value, with a 91 Waukesha Knock Index<sup>®</sup>.

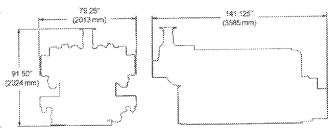
For conditions or fuels other than standard, the Waukesha Engine Sales Engineering Department.

## PERFORMANCE: L7042GL VHP SERIES GAS ENGINES

Englis		O" FICW	85" F	ICW	Metric				
S RPM S	12	00 1000	1200	1000	RPM	1200	1000	1200	1000
Power(E	ho) 14	78 1232	1547	1289	Power (kWb)	1103	919	1154	962
	lu/oho-hri 71	55 6815	7180	6840	BSFC (kJ/kW-hr)	10124	9643	10160	9679
		90 0.90	0.70	0.70	NOx (g/nm²)	0.37	0.37	0.29	0.29
**************************************		75 2.65	2.65	2.55	CO (g/nm²)	1,14	1.10	1.10	1.05
		00 1.00	1,10	1.10	NMHC (g/nm³)	041	0.41	0.45	0.45
BSFC (E	tu/bhp-hr) 69	10 6615	6936	6640	BSFC (kJ/kW-hr)	9778	9360	9813	9396
NOX (or	ms/bhp-hr) 1.	50 1.60	1.30	1.40	NOx (g/nm²)	0.62	0.66	0.54	0.58
	하나는 맛이 많아가는 그 사람이 가게 하는데	00 2.75	2.90	2.65	CO (g/nm²)	1.24	1.14	1.20	1.10
2×3×4		70 1.00	0.80	1.10	NMHC (g/nm³)	0.29	0.41	0.33	0.45

#### NOTES:

- Performance ratings are based on ISO 3046/1-1995 with mechanical efficiency of 90% and Tora limited to ± 10° F.
- Fuel consumptions based on ISO 3046/1-1995 with a +5% tolarance for commercial quality natural gas having a 900 Btu/ft<sup>3</sup> saturated low heat value.
- Data based on standard conditions of 77" F (25" C) embient temperature, 29.53 on sor inches Hg (100kPa) barometric pressure, 30% relative humidity (0.3 inches Hg / (2324 mm) 1 kPa water vapor pressure).
- 4) Data will vary due to variations in site conditions. For conditions and/or fuels other than standard, consult the Waukesha Engine Sales Engineering Department.





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Consuit your local Waukesha Distributor for system application assistance. The manufacturer reserves the right to change or modify without notice, the design or equipment specifications as herein set forth without incurring any obligation either with respect to equipment previously sold or in the process of construction except where otherwise specifically guaranteed by the manufacturer.

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## Waukesha L5794LT Emission Calculations South Ignacio Central Delivery Point Red Cedar Gathering Company

## Waukesha L5794LT - Internal Combustion Engine (4SLB)

Units E5 - E8

Manufacturer Unit Rating:	1,447 hp @ 1,200 rpm
Site Specific Unit Rating <sup>a</sup> :	1,401 hp @ 6,320 ft
BSFC:	7,600 btu/hp-hr
Maximum Heat Input:	10.6 MMBtu/hr
Operating Schedule:	8,760 hr/yr
Maximum Fuel Use <sup>b</sup> :	103.6 mmscf/yr

<sup>&</sup>lt;sup>a</sup> Based on manufacturer's site derate of 2.4% for every 1,000 ft above 5,000 ft elevation.

#### Potential Criteria Pollutant Emissions

		Uncontrolled Emissions							
Pollutant	Emissi	on Factors	Data Source	(lb/hr)	(ton/yr)				
NO <sub>X</sub>	2.08	g/hp-hr	Engine Manufacturer	6.42	28.14				
co	1.84	g/hp-hr	Engine Manufacturer	5.68	24.89				
VOC	1.00	g/hp-hr	Engine Manufacturer	3.09	13.53				
PM <sub>10</sub>	9.99E-03	lb/MMBtu	AP-42; Table 3.2-2	0.11	0.47				
SO <sub>2</sub>	5.88E-04	lb/MMBtu	AP-42; Table 3.2-2	0.01	0.03				
CO <sub>2</sub>	110.00	lb/MMBtu	AP-42; Table 3.2-2	1,171.24	5,130.01				
Methane	1.25	lb/MMBtu	AP-42; Table 3.2-2	13.31	58.30				
CO₂e					5,975.99 MT/yr				

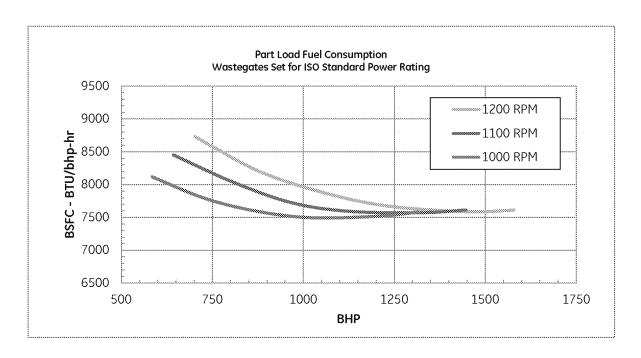
Hazardous Air Pollutant (HAP) Emissions

			Uncontrolled Emissions		
Pollutant	Emission Factors °	Data Source	(lb/hr)	(ton/yr)	
1,3-Butadiene	2.67E-04 lb/MMBtu	AP-42; Table 3.2-2	2.84E-03	1.25E-02	
2,2,4-Trimethylpentane	2.50E-04 lb/MMBtu	AP-42; Table 3.2-2	2.66E-03	1.17E-02	
Acetaldehyde	8.36E-03 lb/MMBtu	AP-42; Table 3.2-2	8.90E-02	0.39	
Acrolein	5.14E-03 lb/MMBtu	AP-42; Table 3.2-2	5.47E-02	0.24	
Benzene	4.40E-04 lb/MMBtu	AP-42; Table 3.2-2	4.68E-03	2.05E-02	
Biphenyl	2.12E-04 lb/MMBtu	AP-42; Table 3.2-2	2.26E-03	9.89E-03	
Formaldehyde	5.28E-02 lb/MMBtu	AP-42; Table 3.2-2	5.62E-01	2.46	
Methanol	2.50E-03 lb/MMBtu	AP-42; Table 3.2-2	2.66E-02	0.12	
n-Hexane	1.11E-03 lb/MMBtu	AP-42; Table 3.2-2	1.18E-02	5.18E-02	
Toluene	4.08E-04 lb/MMBtu	AP-42; Table 3.2-2	4.34E-03	1.90E-02	
Xylene	1.84E-04 lb/MMBtu	AP-42; Table 3.2-2	1.96E-03	8.58E-03	
Total			< 0.76	< 3.34	

c Uncontrolled emission factors for 4-stroke, lean-burn (4SLB) engines based on the highest emission factor between EPA's AP-42, GRI field data and GRI literature data sets, and the manufacturer's data.

<sup>&</sup>lt;sup>b</sup> Based on LHV of: 900 btu/scf

## Engine Ratings and Fuel Consumption ISO Standard (Continuous) Ratings for Model L5794LT with ESM\* 130°F (54°C) Auxiliary Water Temperature



RPM	800	900	1000	1000 <sup>4</sup>	1100	1200
CONTINUOUS BHP	614	954	1206	1272	1326	1447
OVERLOAD BHP	None	None	1315	None	1447	1579

OVERLOAD	Allowed 2 Hour	s per 24 Hours			
STANDARD CONDITIONS	<u>Barometer</u> 29.54 in. Hg. (100 kPa)	<u>Ambient Temperature</u> 77°F (25°C)			
DEDUCTIONS	Altitude: 2.4% per 1000 ft. 130 Ambient Temperature: 2.4% per				
FUEL	Dry Natural Gas – 900 Btu/ft³ Refer to S-7884-7 for				
EQUIPMENT	Engine Equipped with Lube Oil and Coolin	Engine Equipped with Lube Oil and Cooling Water Pumps but without Radiator Fan			
ENGINE DATA  Turbocharged & Intercooled with 130°F (54°C) Intercooler Water 10.2:1 Compression Ratio					

## NOTES:

- 1. ISO Standard (continuous) power ratings conform to ISO 3046/1, latest version, with a mechanical efficiency of 90% and auxiliary water temperature, Tcra, of 130°F (54°C) limited to  $\pm$  10°F ( $\pm$  5.5°C).
- 2. Reference Heat Rejection and Operating Data Standard Sheet S-6124-79.
- 3. Engine set to an exhaust oxygen concentration of 7.8% at ESM ignition timing for 2.25 g/bhp-hr  $NO_x$  (0.91 g/nm<sup>3</sup> @ 5%  $O_z$ ).
- 4. Power generation continuous BHP at 1000 RPM is 1272 BHP @ 7.4% O<sub>2</sub> with no overload allowed.

<sup>\*</sup>Trademark of General Electric Company. All other trademarks are the property of their respective owners.



Engine Ratings & Fuel Consumption
Model L5794LT with ESM

130°F (54°C) Auxiliary Water Temperature
180°F (82°C) Jacket Water Temperature

Ref.
C
977-5

Page 1 of 1

# HEAT REJECTION AND OPERATING DATA — MODEL L5794LT with ESM\* ESM SPARK TIMING for 2.25 g/bhp-hr NO $_{\rm x}$ (0.91 g/nm³ @ 5% O $_{\rm z}$ ), 10.2:1 CR, 7.8% EXHAUST O $_{\rm z}$

## 130°F AUXILIARY WATER TEMP. — 180°F JACKET WATER TEMP.

	ВМЕР	ENGII	ENGINE SPEED - RPM			
	(PSI)	1000	1100	1200		
	180	1315	1447	1579		
	165	1206	1326	1447		
POWER	140	1023	1125	1228		
(BHP)	120	877	965	1052		
	100	731	804	877		
	80	585	643	702		
	180	7448	7478	7476		
	165	7386	7439	7454		
BRAKE SPEC FUEL CONS.	140	7363	7459	7540		
(BTU/BHP-HR)	120	7456	7593	7745		
	100	7651	7903	8062		
	80	7975	8304	8577		
	180	9797	10821	11801		
	165	8906	9867	10786		
FUEL CONS.	140	7533	8395	9258		
(BTU/HR x 1000)	120	6538	7325	8150		
	100	5591	6353	7070		
	80	4662	5340	6018		
	180	2564	2805	3017		
	165	2274	2511	2721		
HEAT TO JACKET WATER	140	1860	2092	2316		
(BTU/HR x 1000)	120	1590	1818	2056		
	100	1356	1601	1822		
	80	1148	1383	1617		
	180	413	464	512		
HEAT TO LUBE OIL	165	387	438	485		
	140	349	400	448		
(BTU/HR x 1000)	120	325	376	425		
	100	306	358	408		
	80	294	347	400		

180   341   429   514     165   315   389   461     165   315   329   386     173   195   216     180   441   452   459     165   419   431   440     165   419   431   440     165   419   431   440     165   419   431   440     165   419   431   440     165   419   431   440     165   419   431   440     165   419   431   440     165   419   431   440     165   366   382   399     100   347   369   386     80   329   353   374     180   2864   3181   3491     165   2600   2897   3187     170   180   2864   3181   3491     165   2600   2897   3187     180   2864   3181   3491     165   2600   2897   3187     180   2192   2457   2733     180   2192   2457   2733     180   1313   1520   1733     180   880   886   893     165   875   882   889     165   875   882   889     165   875   882   889     165   875   882   889     165   875   881   866   878     180   2787   3079   3357     165   2534   2807   3069     1NDUCTION AIR   140   2143   2388   2634     180   2787   3079   3357     165   2534   2807   3069     1NDUCTION AIR   140   2143   2388   2634     180   2787   3079   3357     165   2534   2807   3069     1NDUCTION AIR   140   2143   2388   2634     180   2787   3079   3357     165   2534   2807   3069     1NDUCTION AIR   140   2143   2388   2634     180   2787   3079   3357     165   2534   2807   3069     100   213   247   277     20   245   245     20   245   245     20   245   245     20   245   245     20   245   245     20   245   245     20   245   245     20   245   245     20   245   245     20   245     20   245   245     20   245	ВМЕР	ENGII	NE SPEED -	- RPM
HEAT TO INTERCOOLER (BTU/HR x 1000)  HEAT TO INTERCOOLER (BTU/HR x 1000)  120 245 286 333  100 213 247 277  80 173 195 216  180 441 452 459  165 419 431 440  HEAT TO 140 387 402 414  RADIATION (BTU/HR x 1000)  120 366 382 399  100 347 369 386  80 329 353 374  180 2864 3181 3491  165 2600 2897 3187  180 2864 3181 3491  165 2600 2897 3187  (BTU/HR x 1000)  120 1896 2137 2403  180 165 2600 2897  180 2137 2403  180 880 886 893  165 875 882 889  EXHAUST TEMP AFTER TURBINE (± 50°F)  100 845 857 867  80 821 835 848  180 2787 3079 3357  165 2534 2807 3069  INDUCTION AIR 140 2143 2388 2634  INDUCTION AIR 140 2143 2388 2634  INDUCTION AIR 140 2143 2388 2634	(PSI)	1000	1100	1200
HEAT TO INTERCOOLER (BTU/HR x 1000)  120 245 286 333  100 213 247 277  80 173 195 216  180 441 452 459  165 419 431 440  HEAT TO RADIATION (BTU/HR x 1000)  120 366 382 399  100 347 369 386  80 329 353 374  180 2864 3181 3491  165 2600 2897 3187  180 2864 3181 3491  165 2600 2897 3187  180 2864 3181 3491  165 2600 2897 3187  180 2864 3181 3491  165 2600 2897 3187  180 2864 3181 3491  165 2600 2897 3187  180 886 893  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  165 875 882 889  180 2787 3079 3357  165 2534 2807 3069  1NDUCTION AIR 140 2143 2388 2634	180	341	429	514
INTERCOOLER (BTU/HR x 1000)	165	315	389	461
(BTU/HR x 1000)   120   245   286   333   333   100   213   247   277   80   173   195   216   180   441   452   459   165   419   431   440   452   414   416	 140	275	329	386
80	120	245	286	333
180	100	213	247	277
HEAT TO RADIATION (BTU/HR x 1000)  120 366 382 399 100 347 369 386 80 329 353 374  180 2864 3181 3491 165 2600 2897 3187 165 2600 2897 3187 165 2600 2897 3187 165 2600 2897 3187 165 2600 2897 3187 165 2600 2897 3187 165 2600 2897 3187 165 2600 2897 3187 165 2600 2897 3187 165 2600 2897 3187 160 1607 1844 2070 100 1607 1844 2070 100 1607 1844 2070 100 1607 1844 2070 100 880 880 886 893 165 875 882 889 165 875 882 889 165 875 882 889 165 875 882 889 165 875 882 889 165 875 882 889 165 875 882 889 165 875 882 889 165 875 882 889 165 875 882 889 165 875 867 867 80 821 835 848 180 2787 3079 3357 165 2534 2807 3069 1NDUCTION AIR 140 2143 2388 2634 180 2787 3089 3069	80	173	195	216
HEAT TO RADIATION (BTU/HR x 1000)  120 366 382 399  100 347 369 386  80 329 353 374  180 2864 3181 3491  165 2600 2897 3187  TOTAL ENERGY 140 2192 2457 2733  (BTU/HR x 1000)  120 1896 2137 2403  100 1607 1844 2070  80 1313 1520 1733  180 880 886 893  165 875 882 889  EXHAUST TEMP AFTER TURBINE (± 50°F)  140 866 874 883  160 886 878  180 845 857 867  80 821 835 848  INDUCTION AIR 140 2143 2388 2634  INDUCTION AIR FLOW	180	441	452	459
RADIATION (BTU/HR × 1000)  120  366  382  399  100  347  369  386  80  329  353  374  180  2864  3181  3491  165  2600  2897  3187  TOTAL ENERGY IN EXHAUST (BTU/HR × 1000)  120  1896  2137  2403  100  1607  1844  2070  80  1313  1520  1733  180  880  886  893  165  875  882  889  EXHAUST TEMP AFTER TURBINE (± 50°F)  120  880  821  835  848  180  2787  3079  3357  165  2534  2807  3069  INDUCTION AIR FLOW	165	419	431	440
(BTU/HR x 1000) 120 366 382 399 100 347 369 386 80 329 353 374 180 2864 3181 3491 165 2600 2897 3187 140 2192 2457 2733 187 187 140 1896 2137 2403 100 1607 1844 2070 80 1313 1520 1733 180 880 886 893 165 875 882 889 165 875 882 889 140 866 874 883 160 845 857 867 80 821 835 848 180 2787 3079 3357 165 2534 2807 3069 100 100 2143 2388 2634 180 2143 2443 2443 2443 180 2443 2443 2443 2443 2443	140	387	402	414
80   329   353   374     180   2864   3181   3491     165   2600   2897   3187     165   2600   2897   3187     170TAL ENERGY   140   2192   2457   2733     180   1896   2137   2403     100   1607   1844   2070     80   1313   1520   1733     180   880   886   893     165   875   882   889     165   875   882   889     165   875   882   889     165   876   876   878     100   845   857   867     80   821   835   848     180   2787   3079   3357     165   2534   2807   3069     INDUCTION AIR   140   2143   2388   2634     FLOW   160   2004   2006     180   2787   2388   2634     180   2787   3288     180   2787   3288     180   2787   3288     180   2787   3288     180   2787   3288     180   2787   3288     180   2787   3288     180   2787   3288     180   2787   3288     180   2787   3	120	366	382	399
180   2864   3181   3491     165   2600   2897   3187     170TAL ENERGY   140   2192   2457   2733     180   1896   2137   2403     100   1607   1844   2070     80   1313   1520   1733     180   880   886   893     165   875   882   889     165   875   882   889     165   875   882   889     165   876   876   876     100   845   857   867     80   821   835   848     180   2787   3079   3357     165   2534   2807   3069     1NDUCTION AIR   140   2143   2388   2634     FLOW   100   1007   2007     100   2143   2388   2634     100   2143   2388   2634     2007   2007   2007     2007   2007   2007     2007   2007   2007     2007   2007   2007     2007   2007   2007     2007   2007   2007     2007   2007   2007     2007   2007	100	347	369	386
TOTAL ENERGY 140 2192 2457 2733 187 (BTU/HR × 1000) 120 1896 2137 2403 100 1607 1844 2070 80 1313 1520 1733 165 875 882 889 165 875 882 889 140 866 874 883 AFTER TURBINE (± 50°F) 120 858 866 878 100 845 857 867 80 821 835 848 180 2787 3079 3357 165 2534 2807 3069 1NDUCTION AIR FLOW 100 100 100 100 100 100 100 100 100 10	80	329	353	374
TOTAL ENERGY IN EXHAUST (BTU/HR x 1000)  120 1896 1317 2403 100 1607 1844 2070 80 1313 1520 1733 180 880 886 893 165 875 882 889 EXHAUST TEMP AFTER TURBINE (± 50°F) 120 80 821 835 848 180 82787 80 821 835 848 180 2787 3079 3357 165 2534 2807 3069 1NDUCTION AIR FLOW	180	2864	3181	3491
IN EXHAUST (BTU/HR x 1000)	165	2600	2897	3187
(BTU/HR x 1000) 120 1896 2137 2403 100 1607 1844 2070 80 1313 1520 1733 180 880 886 893 165 875 882 889 EXHAUST TEMP AFTER TURBINE (± 50°F) 120 858 866 878 100 845 857 867 80 821 835 848 180 2787 3079 3357 165 2534 2807 3069 INDUCTION AIR FLOW 100 1607 2143 2388 2634	140	2192	2457	2733
80   1313   1520   1733   180   880   886   893   165   875   882   889   165   875   882   889   140   866   874   883   866   878   120   858   866   878   100   845   857   867   80   821   835   848   180   2787   3079   3357   165   2534   2807   3069   180UCTION AIR   140   2143   2388   2634   180   2634	120	1896	2137	2403
180   880   886   893     165   875   882   889     EXHAUST TEMP   140   866   874   883     AFTER TURBINE   120   858   866   878     100   845   857   867     80   821   835   848     180   2787   3079   3357     165   2534   2807   3069     INDUCTION AIR   140   2143   2388   2634     FLOW   1880   1880   2880   2880     180   2787   3079   3357     165   2534   2807   3069     180   2143   2388   2634     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     180   2143   2388     2143   2388     215   2143   2388     215   2143   2388     215   2143   2388     215   2145   2145     215   215   215     215   215   215     215   215   215     215   215   215     215   215     215   215     215   215     215   215     215   215	100	1607	1844	2070
EXHAUST TEMP AFTER TURBINE (± 50°F)  140  866  874  883  120  858  866  878  100  845  857  867  80  821  835  848  180  2787  3079  3357  165  2534  2807  3069  INDUCTION AIR FLOW	80	1313	1520	1733
EXHAUST TEMP AFTER TURBINE (± 50°F)       140       866       874       883         120       858       866       878         100       845       857       867         80       821       835       848         180       2787       3079       3357         165       2534       2807       3069         INDUCTION AIR FLOW       140       2143       2388       2634	180	880	886	893
AFTER TURBINE (± 50°F) 120 858 866 878 100 845 857 867 80 821 835 848 180 2787 3079 3357 165 2534 2807 3069 INDUCTION AIR FLOW 122 143 2388 2634 1250 1250 1250 1250 1250 1250 1250 1250	165	875	882	889
(±50°F) 120 858 866 878 100 845 857 867 80 821 835 848 180 2787 3079 3357 165 2534 2807 3069 INDUCTION AIR 140 2143 2388 2634 FLOW 1888 1888 1888 1888 1888	140	866	874	883
80   821   835   848     180   2787   3079   3357   165   2534   2807   3069   1NDUCTION AIR   140   2143   2388   2634   FLOW   1868   1869	120	858	866	878
180 2787 3079 3357 165 2534 2807 3069 INDUCTION AIR 140 2143 2388 2634 FLOW 1000 1000 2000 2000	100	845	857	867
165 2534 2807 3069 INDUCTION AIR 140 2143 2388 2634 FLOW 1000 1000 2000 23300	80	821	835	848
INDUCTION AIR 140 2143 2388 2634 FLOW 1000 1000 1000 1000 1000 1000 1000 10	 180	2787	3079	3357
FLOW 2143 2300 2034	165	2534	2807	3069
400   4000   0004   0740	140	2143	2388	2634
(SCFM)   120   1860   2084   2319	120	1860	2084	2319
100 1591 1807 2011	100	1591	1807	2011
80 1326 1519 1712	80	1326	1519	1712

Continued



HEAT REJECTION AND OPERATING DATA MODEL – L5794LT with ESM 130°F AUX. WATER TEMPERATURE 180°F JACKET WATER TEMPERATURE

EN: 128025 DATE: 7/03 Ref. S 6124-79

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# HEAT REJECTION AND OPERATING DATA — MODEL L5794LT with ESM\* ESM SPARK TIMING for 2.25 g/bhp-hr NO $_{\rm x}$ (0.91 g/nm³ @ 5% O $_{\rm z}$ ), 10.2:1 CR, 7.8% EXHAUST O $_{\rm z}$

130°F AUXILIARY WATER TEMP. — 180°F JACKET WATER TEMP.

10	U I AUNI	LIVIVI	VVAIL	.17   [ ]
	ВМЕР	ENGII	NE SPEED -	- RPM
	(PSI)	1000	1100	1200
	180	12517	13825	15077
	165	11378	12606	13780
EXHAUST GAS FLOW	140	9624	10725	11827
(LBS/HR)	120	8353	9357	10412
	100	7143	8117	9033
	80	5956	6822	7688
	180	2.06	2.06	2.07
	165	2.08	2.08	2.08
NO. EMISSION	140	2.11	2.11	2.04
(G/BHP-HR)	120	2.13	2.13	2.00
	100	2.28	2.14	2.07
	80	2.70	2.46	2.23
	180	1.61	1.69	1.77
(CO)	165	1.68	1.76	184
EMISSION	140	1.82	1.90	1.96
(G/BHP-HR)	120	1.95	2.03	2.07
	100	2.15	2.19	2.24
	80	2.50	2.52	2.53

	BMEP	ENGINE SPEED – RPM		
	(PSI)	1000	1100	1200
	180	0.18	0.17	0.16
	165	0.19	0.18	0.17
NMHC EMISSION	140	0.22	0.21	0.20
(G/BHP-HR)	120	0.25	0.24	0.23
***************************************	100	0.28	0.27	0.26
	80	0.33	0.32	0.31
	180	2.41	2.25	2.10
	165	2.59	2.44	2.29
THC	140	2.97	2.82	2.66
EMISSION (G/BHP-HR)	120	3.35	3.20	3.04
	100	3.84	3.68	3.52
	80	4.50	4.34	4.18

## NOTES:

- All data are based on ISO standard conditions of 29.54 inches Hg. barometric pressure, 77°F ambient and induction air temperature, 30%
  relative humidity (0.3 inches Hg. water vapor pressure), 182°F engine jacket water outlet temperature, and ignition timing as provided by
  the Engine System Manager (ESM).
- 2. All data are average values at the standard conditions and will vary for individual engines and with operating and ambient conditions and with changes to ignition timing or air/fuel ratio. An adequate reserve should be used for cooling system or heat recovery calculations. See also Cooling System Guidelines, S-6699-7, latest version.
- 3. ISO Standard (continuous) power ratings conform to ISO 3046/1, latest version, with a mechanical efficiency of 90% and auxiliary water temperature, Tcra, of 130°F limited to ± 10°F.
- 4. Fuel standard: dry natural gas, 900 BTU/scf saturated lower heating value (SLHV), with a minimum Waukesha Knock Index\* of 91. Refer to S-7884-7, latest version, for the full fuel specification.
- 5. 10.2:1 compression ratio.
- 6. For heat rejection changes due to engine jacket water outlet temperature higher than standard (Note 1), refer to S-7613-3, latest version.
- Total Exhaust Energy includes both recoverable and non-recoverable heat. For a procedure to calculate recoverable heat refer to S-8117-2, latest version.
- 8. Exhaust oxygen (O<sub>2</sub>) concentration set to 7.8% at ESM spark timing for 2.25 g/bhp-hr NO<sub>x</sub> (0.91 g/nm³ @ 5% O<sub>2</sub>). This O<sub>2</sub> level is measured at the port located in the exhaust manifold upstream of the turbocharger.
- 9. Reference Engine Ratings and Fuel Consumption Curve Sheet C-977-5, latest version
- 10. Exhaust flow at nominal 29.54 inches Hg. atmospheric pressure:

Flow rate: ACFM = 
$$\frac{\text{(Exh. Flow, lb/hr)} \times \text{(Exh. Temp. }^{\circ}\text{F} + 460^{\circ}\text{)}}{2250}$$

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HEAT REJECTION AND OPERATING DATA

MODEL – L5794LT with ESM

130°F AUX. WATER TEMPERATURE

180°F JACKET WATER TEMPERATURE

Ref.

S

DATE: 7/03

6124-79

## - METRIC -

# HEAT REJECTION AND OPERATING DATA — MODEL L5794LT with ESM\* ESM SPARK TIMING for 0.91 g/nm³ @ 5% O<sub>2</sub> (2.25 g/bhp-hr), 10.2:1 CR, 7.8% EXHAUST O<sub>2</sub>

54°C AUXILIARY WATER TEMP. — 82°C JACKET WATER TEMP.

	BMEP	ENGINE SPEED - RPM			
	(bar)	1000	1100	1200	
	12.42	981	1079	1177	
	11.39	899	989	1079	
POWER	9.66	763	839	916	
(KW)	8.28	654	719	785	
	6.9	545	599	654	
	5.52	436	480	523	
	12.42	10537	10580	10577	
	11.39	10449	10525	10546	
BRAKE SPEC FUEL CONS.	9.66	10417	10553	10668	
(KJ/KWH)	8.28	10548	10742	10957	
	6.9	10824	11182	11407	
	5.52	11283	11748	12135	
	12.42	2872	3172	3459	
	11.39	2610	2892	3161	
FUEL	9.66	2208	2460	2713	
CONS. (KW)	8.28	1916	2147	2389	
	6.9	1639	1862	2072	
	5.52	1367	1565	1764	
	12.42	751	822	884	
	11.39	666	736	798	
HEAT TO	9.66	545	613	679	
JACKET WATER (KW)	8.28	466	533	603	
	6.9	398	469	534	
	5.52	337	405	474	
	12.42	121	136	150	
	11.39	113	128	142	
HEAT TO	9.66	102	117	131	
LUBE OIL (KW)	8.28	95	110	125	
, .	6.9	90	105	120	
	5.52	86	102	117	

	BMEP	ENGI	NE SPEED -	- RPM
	(bar)	1000	1100	1200
	12.42	100	126	151
	11.39	92	114	135
HEAT TO INTERCOOLER	9.66	80	96	113
(KW)	8.28	72	84	97
	6.9	63	73	81
	5.52	51	57	63
	12.42	129	132	135
	11.39	123	126	129
HEAT TO	9.66	113	118	121
RADIATION (KW)	8.28	107	112	117
	6.9	102	108	113
	5.52	97	103	110
	12.42	840	932	1023
	11.39	762	849	934
TOTAL ENERGY	9.66	642	720	801
IN EXHAUST (KW)	8.28	556	626	704
	6.9	471	541	607
	5.52	385	445	508
	12.42	471	475	478
	11.39	468	472	476
EXHAUST TEMP AFTER TURBINE	9.66	464	468	473
(±30°C)	8.28	459	463	470
	6.9	452	458	464
	5.52	438	446	453
	12.42	4284	4732	5160
	11.39	3894	4315	4716
INDUCTION AIR	9.66	3294	3671	4048
FLOW (NM³/HR)	8.28	2859	3203	3564
	6.9	2445	2778	3092
	5.52	2039	2335	2631
<u> </u>		·	·	Captional

Continued



– Metric – HEAT REJECTION AND OPERATING DATA MODEL – L5794LT with ESM 54°C AUX. WATER TEMPERATURE 82°C JACKET WATER TEMPERATURE

EN: 128025 DATE: 7/03 Ref. \_\_\_S \_\_\_6124-79

Page 3 of 4

## - METRIC -

# HEAT REJECTION AND OPERATING DATA — MODEL L5794LT with ESM\* ESM SPARK TIMING for 0.91 g/nm³ @ 5% O<sub>2</sub> (2.25 g/bhp-hr), 10.2:1 CR, 7.8% EXHAUST O<sub>2</sub>

## 54°C AUXILIARY WATER TEMP. — 82°C JACKET WATER TEMP.

	BMEP ENGINE SPEED - RPM			- RPM
	(bar)	1000	1100	1200
	12.42	5678	6271	6839
	11.39	5161	5718	6251
EXHAUST GAS FLOW	9.66	4366	4865	5365
(KG/HR)	8.28	3789	4245	4723
	6.9	3240	3682	4097
	5.52	2702	3095	3487
	12.42	0.83	0.83	0.83
	11.39	0.84	0.84	0.84
NO <sub>x</sub> EMISSION	9.66	0.85	0.85	0.82
(G/NM³ AT 5% O₂)	8.28	0.86	0.86	0.81
	6.9	0.92	0.86	0.83
	5.52	1.09	0.99	0.90
	12.42	0.65	0.68	0.71
	11.39	0.68	0.71	0.74
CO EMISSION	9.66	0.73	0.77	0.79
(G/NM³ AT 5% O₂)	8.28	0.79	0.82	0.83
	6.9	0.87	0.88	0.90
	5.52	1.01	1.01	1.02

	BMEP ENG		GINE SPEED - RPM		
	(bar)	1000	1100	1200	
	12.42	0.07	0.07	0.06	
	11.39	0.08	0.07	0.07	
NMHC EMISSION	9.66	0.09	0.08	0.08	
(G/NM³ AT 5% O₂)	8.28	0.10	0.10	0.09	
	6.9	0.11	0.11	0.11	
	5.52	0.13	0.13	0.12	
	12.42	0.97	0.91	0.85	
	11.39	1.04	0.98	0.92	
THC	9.66	1.20	1.13	1.07	
EMISSION (G/NM³ AT 5% O₂)	8.28	1.35	1.29	1.22	
	6.9	1.54	1.48	1.42	
	5.52	1.81	1.75	1.68	

#### NOTES:

- 1. All data are based on ISO standard conditions of 100 kPa barometric pressure, 25°C ambient and induction air temperature, 30% relative humidity (1 kPa water vapor pressure), 82°C engine jacket water outlet temperature, and ignition timing as provided by the Engine System Manager (ESM).
- 2. All data are average values at the standard conditions and will vary for individual engines and with operating and ambient conditions and with changes to ignition timing or air/fuel ratio. An adequate reserve should be used for cooling system or heat recovery calculations. See also Cooling System Guidelines, S-6699-7, latest version.
- 3. ISO Standard (continuous) power ratings conform to ISO 3046/1, latest version, with a mechanical efficiency of 90% and auxiliary water temperature, Tcra, of 54°C limited to ± 5.5°C.
- 4. Fuel standard: dry natural gas, 35.38 MJ/m³ [25, V (0; 101.325)] saturated lower heating value (SLHV), with a minimum Waukesha Knock Index\* of 91. Refer to S-7884-7, latest version, for the full fuel specification.
- 5. 10.2:1 compression ratio.
- 6. For heat rejection changes due to engine jacket water outlet temperature higher than standard (Note 1), refer to S-7613-3, latest version.
- 7. Total Exhaust Energy includes both recoverable and non-recoverable heat. For a procedure to calculate recoverable heat refer to S-8117-2, latest version
- 8. Exhaust oxygen ( $O_2$ ) concentration set to 7.8% at ESM spark timing for 2.25 g/bhp-hr NO $_x$  (0.91 g/nm $^3$  @ 5%  $O_2$ ). This  $O_2$  level is measured at the port located in the exhaust manifold upstream of the turbocharger.
- 9. Reference Engine Ratings and Fuel Consumption Curve Sheet C-977-5, latest version.
- 10. Exhaust flow at nominal 100 kPa atmospheric pressure:

Flow rate:  $m^3/hr = \frac{(Exh. Flow, kg/hr) \times (Exh. Temp. °C + 273°)}{332.96}$ 

Page 4 of 4



– Metric – HEAT REJECTION AND OPERATING DATA MODEL – L5794LT with ESM 54°C AUX. WATER TEMPERATURE 82°C JACKET WATER TEMPERATURE	EN: 128025 DATE: 7/03	Ref. S 6124-79

<sup>\*</sup>Trademark of General Electric Company. All other trademarks are the property of their respective owners.



## **Analysis Certificate**

Analysis Requested:

GPA 2286\_14

Client: Project #: Red Cedar 95031-0055 Site Name: Compensations: Air & Helium Free South Ignacio Laboratory ID: P904129-01 Date Reported: 05/10/19 Sampled by: K Hunderman Date Sampled: 04/24/19 Analyzed by: I Yazzie / E Montoya Date Received: 04/26/19 Sample Pressure: 409.7 psig Date Analyzed: 05/09/19 Sample Temperature: 67.56 F Analysis Time: Std

<b>GPA</b>	2286	14	report

Components	Mol %	Wt %	L.V. %
Helium	BRL	BRL	BRL
Oxygen	BRL	BRL	BRL
Nitrogen	BRL	BRL	BRL
Carbon Dioxide	4.6651	11.7986	4.6640
Methane	95.0269	87.6072	94.8640
Ethane	0.2657	0.4592	0.4130
Propane	0.0249	0.0632	0.0590
lso-Butane	0.0054	0.0178	BRL
N-Butane	0.0051	0.0172	BRL
so-Pentane	0.0012	0.0052	BRL
N-Pentane	0.0003	0.0011	BRL
so-Hexanes	0.0019	0.0095	BRL
Benzene	0.0001	0.0005	BRL
n-Hexane	BRL	BRL	BRL
so-Heptanes	0.0027	0.0156	BRL
Гoluene	BRL	BRL	BRL
n-Heptane	BRL	BRL	BRL
so-Octanes	0.0004	0.0026	BRL
n-Octane	BRL	BRL	BRL
n-Nonane	BRL	BRL	BRL
so-Decanes	0.0001	0.0008	BRL
n-Decane	BRL	BRL	BRL
<b>Totals</b>	100.0000	100.0000	100.0000



	Analysis Certific	cate	
	Analysis Requested:	GPA 2286_	14
Client:	Red Cedar	Project #:	95031-0055
Site Name:	South Ignacio	Compensations:	Air & Helium Free
Laboratory ID:	P904129-01	Date Reported:	05/10/19
Sampled by:	K Hunderman	Date Sampled:	04/24/19
Analyzed by:	l Yazzie / E Montoya	Date Received:	04/26/19
Sample Pressure:	409.7 psig	Date Analyzed:	05/09/19
Sample Temperature:	67.56 F	Analysis Time:	Sto
	GPA 2261_13 Repo	ort	
Components	Mol %	Wt %	L.V. %
Carbon Dioxide	4.6651	11.7986	4.6640
Hydrogen Sulfide	BRL	BRL	BRL
Nitrogen	BRL	BRL	BRL
Methane	95.0269	87.6072	94.8640
Ethane	0.2657	0.4592	0.4130
Propane	0.0249	0.0632	0.0590
Iso-Butane	0.0054	0.0178	BRL
N-Butane	0.0051	0.0172	BRL
Iso-Pentane	0.0012	0.0052	BRL
N-Pentane	0.0003	0.0011	BRL
C6+	0.0054	0.0305	BRL
Helium	BRL	BRL	BRL
Oxygen	BRL	BRL	BRL
Totals	100.0000	100.0000	100.0000
BRL = Value be	low the method reportable limit = 0.0001%	N/R = Paramet	er not recorded
	Group Reports		
Components	Mol %	Wt %	L.V. %
Hexanes	0.0020	0.0100	BRL
Heptanes	0.0027	0.0156	BRL
Octanes	0.0004	0.0026	BRL
Nonanes	0.0002	0.0015	BRL
Heaviers	0.0001	0.0008	BRL
Totals	0.0054	0.0305	0.0000
C6+	0.0054	0.0305	BRL
C7+	0.0034	0.0205	BRL
C8+	0.0007	0.0049	BRL
C9+	0.0003	0.0023	BRL
BRL = Value be	low the method reportable limit = 0.0001%	N/R = Paramete	er not recorded

5796 US Highway 64, Farmington, NM 87401

Ph (505) 632-0615 Fx (505) 632-1865

errotectus con

Three Springs • 65 Mercado Street, Suite 115, Durango, CO 81301

Ph (970) 259-0615 Fr (800) 362-1879



## **Analysis Certificate**

**Analysis Requested:** 

GPA 2286 14

Client: Project #: Red Cedar 95031-0055 Site Name: Compensations: Air & Helium Free South Ignacio Laboratory ID: P904129-01 Date Reported: 05/10/19 Sampled by: K Hunderman Date Sampled: 04/24/19 Analyzed by: I Yazzie / E Montoya Date Received: 04/26/19 Sample Pressure: 409.7 psig Date Analyzed: 05/09/19 Sample Temperature: 67.56 F Analysis Time: Std

## **Glycal Report**

Components	Mol %	Wt %	L.V. %
Carbon Dioxide	4.6651	11.7986	4.6640
Hydrogen Sulfide	BRL	BRL	BRL
Nitrogen	BRL	BRL	BRL
Methane	95.0269	87.6072	94.8640
Ethane	0.2657	0.4592	0.4130
Propane	0.0249	0.0632	0.0590
lso-Butane	0.0054	0.0178	BRL
N-Butane	0.0051	0.0172	BRL
Iso-Pentane	0.0012	0.0052	BRL
N-Pentane	0.0003	0.0011	BRL
Cyclopentane	BRL	BRL	BRL
n-Hexane	BRL	BRL	BRL
Cyclohexane	BRL	BRL	BRL
Other Hexanes	0.0019	0.0095	BRL
n-Heptane	BRL	BRL	BRL
Methylcyclohexane	0.0005	0.0028	BRL
2,2,4 Trimethylpentane	BRL	BRL	BRL
Benzene	0.0001	0.0005	BRL
Toluene	BRL	BRL	BRL
EthylBenzene	BRL	BRL	BRL
Xylenes	BRL	BRL	BRL
Heaviers	0.0001	0.0008	BRL

BRL = Value below the method reportable limit = 0.0001%

N/R = Parameter not recorded



	Analy	/sis Ce	rtificate	
	Analysis R	Requested:	GPA 2286_14	
Client:	Red Cedar		Project #:	95031-0055
Site Name:	South Ignacio		Compensations:	Air & Helium Free
Laboratory ID:	P904129-01		Date Reported:	05/10/19
Sampled by:	K Hunderman		Date Sampled:	04/24/19
Analyzed by:	l Yazzie / E Montoya		Date Received:	04/26/19
Sample Pressure:	409.7 psig		Date Analyzed:	05/09/19
Sample Temperature:	67.56 F		Analysis Time:	Std
GPA 21	72_09 Report Calcu	lations @	14.696 psia and 60 degrees	5 F
Compressibility Factor Dr	v Gas	0.9979	Compressibility Factor Sat Gas	0.9975
GPM C2+	,	0.084	GPM C3+	0.013
GPM C4+		0.006	GPM C5+	0.002
Ideal Dry Gas Relative De	ensity:	0.601	Ideal Sat Gas Relative Density:	0.59
Real Dry Gas Relative De	•	0.602	Real Sat Gas Relative Density:	0.592
Dry Molecular Weight:	•	17.401	Sat Molecular Weight:	17.098
Gross HV per Ideal Dry ft	3:	965.79	Gross HV per Ideal Sat ft3:	948.94
Gross HV per Real Dry ft3	3:	967.83	Gross HV per Real Sat ft3:	951.32
		C6+ Calculat	ions	
Ideal C6+ Dry Re	elative Density	3.387	C6+ Dry Molecular Weight	98.1
C6+ Compress	ibility Factor	0.873	C6+ Gross HV per Ideal Dry ft3	5376.6
BRL = Value b	pelow the method reportable li	 imit = 0.0001%	N/R = Parameter	not recorded
	<u> </u>			
Drone Zezz	· ~		5/10/20	019
- 21000 DEC 8	9°			
Analyst			Date	
I Yazzie / E Montoya				
Printed				
Comments: 03-21-19 revised	per Khunderman.			
Note: The above analyses are	performed in compliance wit	h GPA 2286_1	4 quality assurance procedures.	
References: GPA 2286_	14, TP-17, GPA Standard	1 2145-09 ar	d GPA Standard 2172-09	

Three Springs × 65 Mercado Street, Suite 115, Durango, CO 81301

GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: South Ignacio - D1

File Name: \\durnetapp101\Shared\Durango Shared\EHS\Air Permits\T5 - South Ignacio\SOU\_Permits\200101\_SOU\_T5\_Renewal App\Dehy\SOU\_D1 PTE (no combustor).ddf

Date: November 01, 2019

## DESCRIPTION:

Description: 30 MMscfd dehy unit; April '19 gas analysis,

gas temp, pressure and max glycol flow (Kim

50015); max gas flow (w/o combustor)

Annual Hours of Operation: 8760.0 hours/yr

#### EMISSIONS REPORTS:

#### UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.5321	12.771	2.3306
Ethane	0.0370	0.887	0.1619
Propane	0.0183	0.439	0.0801
Isobutane	0.0111	0.266	0.0486
n-Butane	0.0164	0.394	0.0718
Isopentane	0.0060	0.145	0.0264
n-Pentane	0.0022	0.052	0.0095
Other Hexanes	0.0259	0.621	0.1133
Methylcyclohexane	0.0735	1.765	0.3221
Benzene	0.0758	1.820	0.3322
C8+ Heavies Total Emissions	0.0352	0.845	0.1542
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	0.8335	20.003	3.6506
	0.2644	6.346	1.1581
	0.0758	1.820	0.3322
	0.0758	1.820	0.3322

#### FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane Ethane Propane Isobutane n-Butane	0.3060 0.0053 0.0012 0.0004 0.0005	7.345 0.128 0.028 0.010 0.011	1.3404 0.0233 0.0050 0.0019 0.0020
Isopentane n-Pentane Other Hexanes Methylcyclohexane Benzene	0.0001 <0.0001 0.0003 0.0001 <0.0001	0.003 0.001 0.008 0.003 <0.001	0.0006 0.0002 0.0014 0.0005 0.0001
C8+ Heavies	<0.0001	<0.001	0.0001
Total Emissions	0.3140	7.537	1.3755
Total Hydrocarbon Emissions	0.3140	7.537	1.3755

				Page: 2
Total VOC	Emissions	0.0027	0.064	0.0118
Total HAP	Emissions	<0.0001	<0.001	0.0001
Total BTEX	Emissions	<0.0001	<0.001	0.0001

## FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane	6.1207	146.896	26.8086
Ethane	0.1064	2.554	0.4661
Propane	0.0230	0.553	0.1009
Isobutane	0.0085	0.204	0.0372
n-Butane	0.0093	0.222	0.0405
Isopentane	0.0028	0.067	0.0122
n-Pentane	0.0008	0.019	0.0034
Other Hexanes	0.0063	0.152	0.0278
Methylcyclohexane	0.0024	0.056	0.0103
Benzene	0.0004	0.010	0.0018
C8+ Heavies	0.0002	0.006	0.0011
Total Emissions	6.2808	150.738	27.5098
Total Hydrocarbon Emissions	6.2808	150.738	27.5098
Total VOC Emissions	0.0537	1.288	0.2351
Total HAP Emissions	0.0004	0.010	0.0018
Total BTEX Emissions	0.0004	0.010	0.0018

## COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Ethane Propane Isobutane	0.8381 0.0423 0.0194 0.0115 0.0169	1.015 0.466 0.276	0.1852 0.0851 0.0504
Other Hexanes Methylcyclohexane	0.0022 0.0262	0.628 1.768	0.0097 0.1146 0.3226
	0.0352		
Total Emissions  Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	1.1475 0.2671	27.540 6.410 1.821	5.0261 1.1698 0.3323

## COMBINED REGENERATOR VENT/FLASH GAS EMISSION CONTROL REPORT:

\_\_\_\_\_

Component	Uncontro tons		ed % Reduction
E	Ethane 0.	.1392 3.67 .6280 0.18 .1809 0.08	52 70.51

Isobutane n-Butane	0.0857 0.1123	0.0504 0.0738	Page: 3 41.17 34.27
Isopentane n-Pentane Other Hexanes Methylcyclohexane Benzene	0.0386 0.0129 0.1411 0.3324 0.3340	0.0270 0.0097 0.1146 0.3226 0.3323	30.02 25.05 18.73 2.94 0.51
C8+ Heavies	0.1553	0.1542	0.66
Total Emissions	31.1604	5.0261	83.87
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	31.1604 1.3932 0.3340 0.3340	5.0261 1.1698 0.3323 0.3323	83.87 16.03 0.51 0.51

#### EQUIPMENT REPORTS:

#### ABSORBER

Specified Absorber Stages: 1.30
Calculated Dry Gas Dew Point: 1.60 lbs. H2O/MMSCF
Temperature: 67.6 deg. F
Pressure: 409.7 psig

Dry Gas Flow Rate: 30.0000 MMSCF/day
Glycol Losses with Dry Gas: 0.0279 lb/hr
Wet Gas Water Content: Saturated
Calculated Wet Gas Water Content: 42.73 lbs. H2O/MMSCF
Calculated Lean Glycol Recirc. Ratio: 9.68 gal/lb H2O

Component	Remaining in Dry Gas	
Water	3.73%	96.27%
Carbon Dioxide	99.75%	0.25%
Methane	99.99%	0.01%
Ethane	99.95%	0.05%
Propane	99.89%	0.11%
Tarahaataa	00 019	0 100
Isobutane	99.81%	0.19%
n-Butane	99.74%	0.26%
Isopentane	99.69%	0.31%
n-Pentane	99.59%	0.41%
Other Hexanes	99.40%	0.60%
Methylcyclohexane	95.31%	4.69%
Benzene	70.37%	
C8+ Heavies	93.68%	6.32%

#### FLASH TANK

Flash Control: Combustion device

Flash Control Efficiency: 95.00 %
Flash Temperature: 100.0 deg. F
Flash Pressure: 30.0 psig

Left in Removed in Component Glycol Flash Gas

Water Carbon Dioxide	99.99% 56.18%	0.01% 43.82%
Methane	8.00%	92.00%
Ethane	25.78%	74.22%
Propane	44.26%	55.74%
Isobutane	56.66%	43.34%
n-Butane	63.92%	36.08%
Isopentane	68.55%	31.45%
n-Pentane	73.76%	26.24%
Other Hexanes	80.49%	19.51%
Methylcyclohexane Benzene C8+ Heavies	97.03% 99.49% 99.39%	2.97% 0.51% 0.61%

#### REGENERATOR

\_\_\_\_\_\_

No Stripping Gas used in regenerator.

Component	Remaining in Glycol	Distilled Overhead
Water Carbon Dioxide Methane Ethane Propane	57.66% 0.00% 0.00% 0.00% 0.00%	42.34% 100.00% 100.00% 100.00% 100.00%
Isobutane	0.00%	100.00%
n-Butane	0.00%	100.00%
Isopentane	0.73%	99.27%
n-Pentane	0.68%	99.32%
Other Hexanes	1.24%	98.76%
Methylcyclohexane	4.12%	95.88%
Benzene	5.03%	94.97%
C8+ Heavies	12.10%	87.90%

## STREAM REPORTS:

## WET GAS STREAM

-----

Temperature: 67.56 deg. F Pressure: 424.40 psia Flow Rate: 1.25e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Methane Ethane	9.00e-002 4.66e+000 9.49e+001 2.65e-001 2.49e-002	6.77e+003 5.02e+004 2.63e+002
n-Butane Isopentane	5.40e-003 5.10e-003 1.20e-003 3.00e-004	9.77e+000 2.85e+000

Other Hexanes 1.90e-003 5.40e+000

Methylcyclohexane 5.00e-004 1.62e+000 Benzene 9.99e-005 2.57e-001 C8+ Heavies 9.99e-005 5.61e-001

Total Components 100.00 5.74e+004

#### DRY GAS STREAM

\_\_\_\_\_

Temperature: 67.56 deg. F Pressure: 424.40 psia Flow Rate: 1.25e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Methane Ethane	3.37e-003 4.65e+000 9.50e+001 2.66e-001 2.49e-002	6.75e+003 5.02e+004 2.63e+002
n-Butane Isopentane	2.99e-004	9.74e+000 2.84e+000 7.10e-001
Methylcyclohexane Benzene C8+ Heavies	7.04e-005	1.81e-001
Total Components	100.00	5.73e+004

## LEAN GLYCOL STREAM

-----

Temperature: 67.56 deg. F Flow Rate: 8.30e+000 gpm

Component		Loading (lb/hr)
Water Carbon Dioxide Methane	9.85e+001 1.50e+000 3.55e-011 4.78e-018 1.45e-009	7.01e+001 1.66e-009 2.24e-016
Isobutane n-Butane Isopentane	3.60e-011 1.26e-011 1.36e-011 9.48e-007 3.18e-007	5.87e-010 6.36e-010 4.43e-005
Other Hexanes Methylcyclohexane Benzene C8+ Heavies	6.77e-005 8.59e-005	3.16e-003 4.01e-003
Total Components	100.00	4.67e+003

#### RICH GLYCOL STREAM

-----

Temperature: 67.56 deg. F Pressure: 424.40 psia Flow Rate: 8.45e+000 gpm

NOTE: Stream has more than one phase.

Component	Conc. (wt%)	Loading (lb/hr)
Water Carbon Dioxide Methane	9.69e+001 2.56e+000 3.50e-001 1.40e-001 3.02e-003	1.22e+002 1.66e+001 6.65e+000
Isobutane n-Butane Isopentane	8.70e-004 4.12e-004 5.40e-004 1.87e-004 6.25e-005	1.96e-002 2.56e-002 8.86e-003
Other Hexanes Methylcyclohexane Benzene C8+ Heavies	1.66e-003 1.69e-003	8.03e-002
Total Components	100.00	4.75e+003

## FLASH TANK OFF GAS STREAM

\_\_\_\_\_

Temperature: 100.00 deg. F Pressure: 44.70 psia Flow Rate: 2.09e+002 scfh

Component	Conc. (vol%)	Loading (lb/hr)	
Carbon Dioxide Methane Ethane	1.23e-001 2.99e+001 6.91e+001 6.41e-001 9.46e-002	7.28e+000 6.12e+000 1.06e-001	
n-Butane Isopentane	1.95e-003	9.25e-003 2.79e-003 7.79e-004	
Methylcyclohexane Benzene C8+ Heavies	9.54e-004	4.12e-004	
Total Components	100.00	1.36e+001	

#### FLASH TANK GLYCOL STREAM

-----

Temperature: 100.00 deg. F Flow Rate: 8.42e+000 gpm

Component Conc. Loading (wt%) (lb/hr)

TEG 9.72e+001 4.60e+003
Water 2.57e+000 1.22e+002
Carbon Dioxide 1.97e-001 9.33e+000
Methane 1.12e-002 5.32e-001

Ethane 7.81e-004 3.70e-002

Propane 3.86e-004 1.83e-002 Isobutane 2.34e-004 1.11e-002 n-Butane 3.46e-004 1.64e-002 Isopentane 1.28e-004 6.07e-003 n-Pentane 4.62e-005 2.19e-003

Other Hexanes 5.53e-004 2.62e-002 Methylcyclohexane 1.62e-003 7.67e-002 Benzene 1.69e-003 7.99e-002

C8+ Heavies 8.46e-004 4.01e-002

Total Components 100.00 4.73e+003

#### FLASH GAS EMISSIONS

\_\_\_\_\_

Flow Rate: 4.92e+002 scfh

Control Method: Combustion Device

Control Efficiency: 95.00

Component Conc. Loading (vol%) (lb/hr) Water 5.70e+001 1.33e+001 Carbon Dioxide 4.15e+001 2.37e+001 Methane 1.47e+000 3.06e-001 Ethane 1.36e-002 5.32e-003 Propane 2.01e-003 1.15e-003 Isobutane 5.62e-004 4.24e-004 n-Butane 6.14e-004 4.63e-004 Isopentane 1.49e-004 1.39e-004 n-Pentane 4.16e-005 3.89e-005 Other Hexanes 2.84e-004 3.17e-004 Methylcyclohexane 9.22e-005 1.18e-004 Benzene 2.03e-005 2.06e-005 C8+ Heavies 5.58e-006 1.23e-005 Total Components 100.00 3.73e+001

#### REGENERATOR OVERHEADS STREAM

\_\_\_\_\_\_

Temperature: 212.00 deg. F Pressure: 14.70 psia Flow Rate: 1.18e+003 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Methane Ethane	9.20e+001 6.82e+000 1.07e+000 3.96e-002 1.33e-002	9.33e+000 5.32e-001 3.70e-002
n-Butane Isopentane	9.70e-004	1.64e-002 6.03e-003 2.17e-003
Methylcyclohexane Benzene C8+ Heavies	3.12e-002	7.58e-002

Page: 8

Total Components 100.00 6.16e+001

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: South Ignacio - D1

File Name: \\durnetapp101\Shared\Durango Shared\EHS\Air Permits\T5 - South

 ${\tt Ignacio \setminus SOU\_Permits \setminus 200101\_SOU\_T5\_Renewal\_App \setminus Dehy \setminus SOU\_D1\_PTE \ (no\_combustor).ddf}$ 

Date: November 01, 2019

DESCRIPTION:

\_\_\_\_\_\_

Description: 30 MMscfd dehy unit; April '19 gas analysis,

gas temp, pressure and max glycol flow (Kim

50015); max gas flow (w/o combustor)

Annual Hours of Operation: 8760.0 hours/yr

WET GAS:

\_\_\_\_\_\_

Temperature: 67.56 deg. F
Pressure: 409.70 psig
Wet Gas Water Content: Saturated

Component	Conc. (vol %)
Carbon Dioxide	4.6651
Methane	95.0269
Ethane	0.2657
Propane	0.0249
Isobutane	0.0054
n-Butane	0.0051
Isopentane	0.0012
n-Pentane	0.0003
Other Hexanes	0.0019
Methylcyclohexane	0.0005
Benzene C8+ Heavies	0.0001

DRY GAS:

Flow Rate: 30.0 MMSCF/day Absorber Stages: 1.3

LEAN GLYCOL:

Glycol Type: TEG

Water Content: 1.5 wt% H2O Flow Rate: 8.3 gpm

PUMP:

Glycol Pump Type: Electric/Pneumatic

FLASH TANK:

Page: 2

Flash Control: Combustion device Flash Control Efficiency: 95.00 % Temperature: 100.0 deg. F Pressure: 30.0 psig



**ELECTRIC PUMPS** 

#### APPLICATIONS:

 Circulating pump for gas glycol dehydrators, gas amine units and other pumping applications.

#### FEATURES:

- No Gas Emissions
- · No Packing
- · Hydraulically Balanced Diaphragms
- . Double-ended Shaft
- Stud Extenders for easy Head Installation
- · Pulse-Free flow
- · Direct or Belt Driven

## SPECIFICATIONS:

 Capacity @ max. pressure: rpm gpm I/min 1500 psi (103 bar) 1200 8.3 31.4

RPM: 1200 max.- 200 min.

Inlet

250 psi max

Connections:
 Inlet: 1" NPT

Outlet: 3/4" NPT

Temperature:

Max: 250° F (121.1° C) Min: 40° F (4.4° C)

[contact factory for temperatures below 40° F (4.4° C)]

Fluid End Material, Manifold: SA395 / SA479

· Elastomers: Highly Saturated Nitrile

Oil Capacity: 2.75 quarts KIMRAY Part No. 7266

2.60 Liters

Weight (dry): 100 lbs (45.7 kg)

· Bi Directional Shaft Rotation

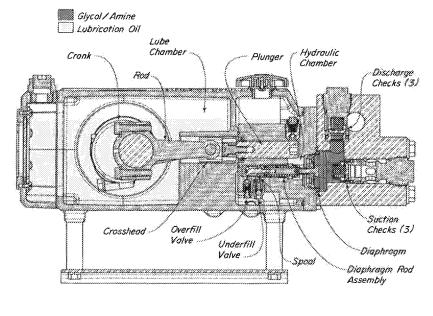
#### **OPERATION:**

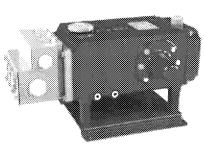
The KIMRAY ELECTRIC GLYCOL PUMP is a uniquely designed hydraulically balanced diaphragm/plunger positive displacement pump. Power to the pump is provided by a properly sized and specified electric motor either directly connected or belt driven. PLUNGERS are utilized to energize DIAPHRAGMS which in turn pressurize glycol/amine solutions used in gas processing. The Plungers operate and are lubricated in clean oil isolated from the process fluids by DIAPHRAGMS. The DIAPHRAGMS are in contact with the hydraulic oil on one side and the glycol/amine solution and on the other side. KIMZOIL EGP1 is a hydraulic/lubrication oil designed for high end pump performance designed for this application. This design allows for the protection of the reciprocating pumping internals from the process fluids.

As shown in the diagram, the PLUNGER(S) are connected to the CROSSHEAD(s) and displace the oil (YELLOW) in the HYDRAULIC CHAMBER as they reciprocate. As the Plunger moves to the right on the pressure stroke, oil is displaced in the Hydraulic Chamber and forces the DIAPHRAGM(s) to move to the right. The Diaphragm movement displaces the glycol/amine solution (GREEN) on the opposing side of the Diaphragm and forces it through the DISCHARGE CHECK VALVE(s). During the pressure stroke, a small amount of oil (YELLOW) leaks past the clearance between the Plunger and cylinder.

As the Plunger moves back on the suction stroke, the pressure drops in the Hydraulic Chamber and a small amount of oil is drawn in through the UNDER-FILL VALVE to replace the oil lost during the pressure stroke. The position of the Spool Valve regulates how much oil is drawn in. The SPOOL VALVE is positioned by the DIAPHRAGM ROD ASSEMBLY which is connected to the Diaphragm. The cycle then repeats.

When the Diaphragm moves too far forward, the Under-Fill port closes and the Over-Fill port opens. The Under-Fill Valve is a check valve that lets oil in during the suction stroke, but will not allow oil to leave. The OVER-FILL VALVE is a check valve that lets oil out during the pressure stroke, but prevents oil from coming in. The spool valve position opens the port to one of the two valves depending on the need for more or less oil.





Kimray is an ISO 9001- certified manufacturer

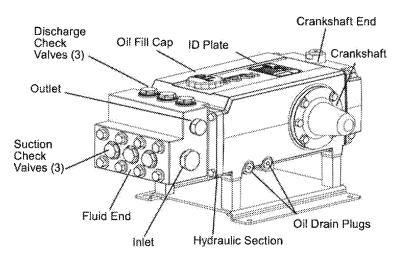
Current Revision: Change Elestomers

www.kimrav.com

G:20.1 Issued 8/16 ELECTRIC PUMPS OVERVIEW



## Component Identification



#### LOCATION:

Locate the pump as close to the fluid supply source as possible.

Allow room for checking the oil level, changing the oil (two drain plugs on the bottom and back of pump), and removing the pump head components (inlet and discharge retainer plates, manifold, and related items).

#### MOUNTING

The pump shaft can rotate in either direction.

To prevent vibration, mount the pump and motor securely on a level rigid base.

On a belt-drive system, align the sheaves accurately; poor alignment wastes horsepower and shortens the belt and bearing life. Make sure the belts are properly tightened, as specified by the belt manufacturer.

On a direct-drive system, align the shafts accurately. Unless otherwise specified by the coupling manufacturer, maximum parallel misalignment should not exceed 0.015 in. (0.4 mm) and angular misalignment should be held to 1° maximum. Careful alignment extends life of the coupling, pump, shafts, and support bearings. Consult coupling manufacturer for exact alignment tolerances

## PUMPS AVAILABLE:

CAT.	TYPE	OPER, PRESS	OPER, PRESS.
NO.		MINIMUM	MAXIMUM
GEA	50015 EV	0	1500

## REPAIR KITS AVAILABLE

CAT.

NO. TYPE **MATERIAL** RZAHSN CHECK VALVE REPAIR KIT HIGHLY SATURATED NITRILE **RZBHSN** COMPLETE REPAIR KIT HIGHLY SATURATED NITRILE RZCHSN DIAPHRAGM REPAIR KIT HIGHLY SATURATED NITRILE

## OIL AVAILABLE:

CAT.		CAPACITY	CAPACITY
NO.	TYPE	QUARTS	LITERS
7266	EGP1 KIMZOIL	2.75	2.60

#### **ACCESSORIES**

Consult installation drawing above for typical system components. Contact KIMRAY INC, or the distributor in your area for more

#### IMPORTANT PRECAUTIONS

Adequate Fluid Supply. To avoid cavitation and premature pump failure, be sure that the pump will have an adequate fluid supply and that the inlet line will not be obstructed.

Positive Displacement. This is a positive-displacement pump. Install a relief valve downstream from the pump.

Safety Guards, Install adequate safety guards over all pulleys, belts, and couplings. Follow all codes and regulations regarding installation and operation of the pumping system.

Shul-Off Valves. Never install shul-off valves between the pump and discharge pressure regulator, relief valve, or in the regulator bypass line.

Freezing Conditions. Protect the pump from freezing. See also the Maintenance Section.

Consult the Factory for the following situations:

- Extreme temperature applications above 250° F (82° C) or below 40° F (4.4° C)
- Viscous fluid applications above 100 Cps
- Chemical compatibility problems
- Hot ambient temperatures above 110° F (43° C)
- Conditions where pump oil may exceed 200° F (93° C) because of a combination of hot ambient temperatures, hot fluid temperature, and full horsepower load - an oil cooler may be required
- Pump RPM less than 200

## CALCULATING REQUIRED HORSEPOWER (KW)\*

gpm x psi = electric motor HP\* 1,460 lpm x bar ~= electric motor kW\*

\* HP/kW is required application power.

When sizing motors with variable speed drives (VFDs), it is very important to select a motor and a VFD rated for constant torque inverter duty service and that the motor is rated to meet the lorque requirements of the pump throughout desired speed range.

Kimray is an ISO 9001- certified manufacturer.

G:20.2 **Issued 2/16** 

Current Revision www.kimray.com Change Kit codes

GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: South Ignacio - D2

File Name: \\durnetapp101\Shared\Durango Shared\EHS\Air Permits\T5 - South Ignacio\SOU\_Permits\200101\_SOU\_T5\_Renewal App\Dehy\SOU\_D2 PTE (no combustor).ddf

Date: November 01, 2019

## DESCRIPTION:

Description: 40 MMscfd dehy unit; April '19 gas analysis, gas temp, pressure and max glycol flow (3

Kim 20015); max gas flow, (no combustor)

Annual Hours of Operation: 8760.0 hours/yr

#### EMISSIONS REPORTS:

## UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.8102	19.446	3.5489
Ethane	0.0225	0.541	0.0987
Propane	0.0094	0.225	0.0410
Isobutane	0.0056	0.135	0.0246
n-Butane	0.0086	0.206	0.0375
Isopentane	0.0033	0.079	0.0143
n-Pentane	0.0012	0.030	0.0055
Other Hexanes	0.0165	0.396	0.0722
Methylcyclohexane	0.0758	1.820	0.3322
Benzene	0.0905	2.171	0.3962
C8+ Heavies Total Emissions	0.0411	0.987  26.035	0.1802 4.7514
Total Hydrocarbon Emissions	1.0848	26.035	4.7514
Total VOC Emissions	0.2520	6.048	1.1038
Total HAP Emissions	0.0905	2.171	0.3962
Total BTEX Emissions	0.0905	2.171	0.3962

#### FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane Ethane Propane Isobutane n-Butane	3.2025 0.0224 0.0041 0.0015 0.0017	76.860 0.537 0.098 0.036 0.040	14.0269 0.0980 0.0178 0.0065 0.0073
Isopentane n-Pentane Other Hexanes Methylcyclohexane Benzene	0.0005 0.0002 0.0014 0.0008 0.0002	0.013 0.004 0.034 0.020 0.004	0.0023 0.0007 0.0062 0.0037 0.0007
C8+ Heavies	0.0001	0.002	0.0004
Total Emissions	3.2353	77.647	14.1706
Total Hydrocarbon Emissions	3.2353	77.647	14.1706

				Page: 2
Total VOC	Emissions	0.0104	0.250	0.0457
Total HAP	Emissions	0.0002	0.004	0.0007
Total BTEX	Emissions	0.0002	0.004	0.0007

## FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane	64.0499	1537.198	280.5386
Ethane	0.4476	10.742	1.9605
Propane	0.0813	1.952	0.3562
Isobutane	0.0296	0.711	0.1298
n-Butane	0.0333	0.800	0.1460
Isopentane	0.0105	0.253	0.0462
n-Pentane	0.0031	0.075	0.0136
Other Hexanes	0.0283	0.679	0.1239
Methylcyclohexane	0.0169	0.407	0.0742
Benzene	0.0034	0.081	0.0148
C8+ Heavies	0.0020	0.048	0.0088
Total Emissions	64.7061	1552.946	283.4126
Total Hydrocarbon Emissions	64.7061	1552.946	283.4126
Total VOC Emissions	0.2086	5.006	0.9135
Total HAP Emissions	0.0034	0.081	0.0148
Total BTEX Emissions	0.0034	0.081	0.0148

## COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Propane Isobutane	4.0127 0.0449 0.0134 0.0071 0.0102	1.078 0.322	0.1967
Other Hexanes	0.0038 0.0014 0.0179 0.0767 0.0906	0.034 0.430	0.0061 0.0784 0.3359
C8+ Heavies	0.0412	0.990	0.1806
Total Emissions	4.3201	103.682	18.9220
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions		103.682 6.299 2.175 2.175	

## COMBINED REGENERATOR VENT/FLASH GAS EMISSION CONTROL REPORT:

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Component	Uncontrolled tons/yr	Controlled tons/yr	% Reduction
Methar	ne 2.0591	17.5758	93.81
Ethar		0.1967	90.45
Propar		0.0589	85.18

Isobutane n-Butane	0.1544 0.1836	0.0311 0.0448	Page: 3 79.86 75.58
Isopentane n-Pentane Other Hexanes Methylcyclohexane Benzene	0.0605 0.0191 0.1962 0.4064 0.4110	0.0167 0.0061 0.0784 0.3359 0.3970	72.49 67.79 60.01 17.35 3.42
C8+ Heavies	0.1889	0.1806	4.42
Total Emissions	288.1640	18.9220	93.43
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	288.1640 2.0174 0.4110 0.4110	18.9220 1.1495 0.3970 0.3970	93.43 43.02 3.42 3.42

#### EQUIPMENT REPORTS:

#### ABSORBER

Specified Absorber Stages: 1.25
Calculated Dry Gas Dew Point: 1.74 lbs. H2O/MMSCF
Temperature: 67.6 deg. F
Pressure: 409.7 psig

Dry Gas Flow Rate: 409.7 psig

Dry Gas Flow Rate: 42.0000 MMSCF/day

Glycol Losses with Dry Gas: 0.0390 lb/hr

Wet Gas Water Content: Saturated

Calculated Wet Gas Water Content: 42.73 lbs. H2O/MMSCF

Calculated Lean Glycol Recirc. Ratio: 8.36 gal/lb H2O

Component	Remaining in Dry Gas	
Water	4.06%	95.94%
Carbon Dioxide	99.79%	0.21%
Methane	99.99%	0.01%
Ethane	99.95%	0.05%
Propane	99.90%	0.10%
Isobutane	99.84%	0.16%
n-Butane	99.77%	0.23%
Isopentane	99.73%	0.27%
n-Pentane	99.64%	0.36%
Other Hexanes	99.49%	0.51%
Methylcyclohexane	95.98%	4.02%
Benzene	74.04%	25.96%
C8+ Heavies	94.59%	5.41%

#### FLASH TANK

Flash Control: Combustion device

Flash Control Efficiency: 95.00 %
Flash Temperature: 100.0 deg. F
Flash Pressure: 30.0 psig

Left in Removed in Component Glycol Flash Gas

Water	99.93%	0.07%
Carbon Dioxide	15.76%	84.24%
Methane	1.25%	98.75%
Ethane	4.79%	95.21%
Propane	10.33%	89.67%
Isobutane	15.94%	84.06%
n-Butane	20.44%	79.56%
Isopentane	23.99%	76.01%
n-Pentane	28.94%	71.06%
Other Hexanes	37.37%	62.63%
Methylcyclohexane	82.46%	17.54%
Benzene	96.58%	3.42%
C8+ Heavies	95.90%	4.10%

#### REGENERATOR

\_\_\_\_\_\_

No Stripping Gas used in regenerator.

Component	Remaining in Glycol	Distilled Overhead
Water	54.06%	45.94%
Carbon Dioxide	0.00%	100.00%
Methane	0.00%	100.00%
Ethane	0.00%	100.00%
Propane	0.00%	100.00%
Isobutane	0.00%	100.00%
n-Butane	0.00%	100.00%
Isopentane	1.60%	98.40%
n-Pentane	1.41%	98.59%
Other Hexanes	2.31%	97.69%
Methylcyclohexane	4.76%	95.24%
Benzene	5.16%	94.84%
C8+ Heavies	12.38%	87.62%

## STREAM REPORTS:

\_\_\_\_\_\_

## WET GAS STREAM

Temperature: 67.56 deg. F Pressure: 424.40 psia Flow Rate: 1.75e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Methane Ethane	9.00e-002 4.66e+000 9.49e+001 2.65e-001 2.49e-002	9.47e+003 7.03e+004 3.69e+002
n-Butane Isopentane	5.40e-003 5.10e-003 1.20e-003 3.00e-004	1.37e+001 3.99e+000

Other Hexanes 1.90e-003 7.55e+000

Methylcyclohexane 5.00e-004 2.26e+000 Benzene 9.99e-005 3.60e-001

C8+ Heavies 9.99e-005 7.86e-001

Total Components 100.00 8.03e+004

### DRY GAS STREAM

\_\_\_\_\_

Temperature: 67.56 deg. F Pressure: 424.40 psia Flow Rate: 1.75e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Carbon Dioxide Methane Ethane	3.66e-003 4.66e+000 9.50e+001 2.66e-001 2.49e-002	9.45e+003 7.03e+004 3.68e+002
n-Butane Isopentane	2.99e-004	1.36e+001 3.98e+000 9.95e-001
Methylcyclohexane Benzene C8+ Heavies	7.41e-005	2.67e-001
Total Components	100.00	8.02e+004

## LEAN GLYCOL STREAM

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Temperature: 67.56 deg. F Flow Rate: 1.00e+001 gpm

Component	Conc. (wt%)	Loading (lb/hr)
Water Carbon Dioxide Methane	9.85e+001 1.50e+000 3.55e-011 4.77e-018 1.44e-009	8.45e+001 2.00e-009 2.69e-016
Isobutane n-Butane Isopentane	3.59e-011 1.25e-011 1.36e-011 9.46e-007 3.17e-007	7.06e-010 7.65e-010 5.32e-005
Other Hexanes Methylcyclohexane Benzene C8+ Heavies	6.73e-005 8.75e-005	4.92e-003
Total Components	100.00	5.63e+003

#### RICH GLYCOL AND PUMP GAS STREAM

\_\_\_\_\_

Temperature: 67.56 deg. F
Pressure: 424.40 psia
Flow Rate: 1.03e+001 gpm
NOTE: Stream has more than one phase.

Component	Conc. (wt%)	Loading (lb/hr)
Wate Carbon Dioxid Methar	GG 9.57e+001 er 2.70e+000 de 4.77e-001 de 1.12e+000 de 8.11e-003	1.56e+002 2.76e+001 6.49e+001
Isobutar n-Butar Isopentar	ne 1.56e-003 ne 6.08e-004 ne 7.23e-004 ne 2.39e-004 ne 7.55e-005	3.53e-002 4.19e-002 1.39e-002
		9.66e-002 9.88e-002
Total Component	s 100.00	5.80e+003

#### FLASH TANK OFF GAS STREAM

\_\_\_\_\_

Temperature: 100.00 deg. F Pressure: 44.70 psia Flow Rate: 1.73e+003 scfh

Component		Loading (lb/hr)
Carbon Dioxide Methane Ethane	1.31e-001 1.16e+001 8.78e+001 3.27e-001 4.06e-002	2.33e+001 6.40e+001 4.48e-001
n-Butane Isopentane	9.48e-004	3.33e-002 1.05e-002 3.11e-003
Methylcyclohexane Benzene C8+ Heavies	9.52e-004	3.38e-003
Total Components	100.00	8.81e+001

#### FLASH TANK GLYCOL STREAM

\_\_\_\_\_

Temperature: 100.00 deg. F Flow Rate: 1.02e+001 gpm

Component Conc. Loading (wt%) (lb/hr) TEG 9.72e+001 5.55e+003 Water 2.74e+000 1.56e+002 Carbon Dioxide 7.63e-002 4.36e+000 Methane 1.42e-002 8.10e-001 Ethane 3.95e-004 2.25e-002

Propane 1.64e-004 9.37e-003 Isobutane 9.85e-005 5.62e-003 n-Butane 1.50e-004 8.57e-003 Isopentane 5.83e-005 3.33e-003 n-Pentane 2.22e-005 1.27e-003

Other Hexanes 2.96e-004 1.69e-002 Methylcyclohexane 1.40e-003 7.96e-002 Benzene 1.67e-003 9.54e-002

C8+ Heavies 8.23e-004 4.69e-002

Total Components 100.00 5.71e+003

#### FLASH GAS EMISSIONS

\_\_\_\_\_

Flow Rate: 4.64e+003 scfh

Control Method: Combustion Device

Control Efficiency: 95.00

Component Conc. Loading (vol%) (lb/hr) Water 6.26e+001 1.38e+002 Carbon Dioxide 3.57e+001 1.92e+002 Methane 1.63e+000 3.20e+000 Ethane 6.09e-003 2.24e-002 Propane 7.55e-004 4.07e-003 Isobutane 2.09e-004 1.48e-003 n-Butane 2.35e-004 1.67e-003 Isopentane 5.98e-005 5.27e-004 n-Pentane 1.76e-005 1.55e-004 Other Hexanes 1.34e-004 1.41e-003 Methylcyclohexane 7.06e-005 8.47e-004 Benzene 1.77e-005 1.69e-004 C8+ Heavies 4.82e-006 1.00e-004 Total Components 100.00 3.33e+002

#### REGENERATOR OVERHEADS STREAM

Temperature: 212.00 deg. F Pressure: 14.70 psia Flow Rate: 1.57e+003 scfh

Conc. Loading (vol%) (lb/hr) Component Water 9.63e+001 7.18e+001 Carbon Dioxide 2.39e+000 4.36e+000 Methane 1.22e+000 8.10e-001 Ethane 1.81e-002 2.25e-002 Propane 5.13e-003 9.37e-003 Isobutane 2.34e-003 5.62e-003 n-Butane 3.56e-003 8.57e-003 Isopentane 1.10e-003 3.28e-003 n-Pentane 4.18e-004 1.25e-003 Other Hexanes 4.62e-003 1.65e-002 Methylcyclohexane 1.87e-002 7.58e-002 Benzene 2.80e-002 9.05e-002 C8+ Heavies 5.83e-003 4.11e-002

Page: 8

Total Components 100.00 7.72e+001

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: South Ignacio - D2

File Name: \\durnetapp101\Shared\Durango Shared\EHS\Air Permits\T5 - South

 ${\tt Ignacio \setminus SOU\_Permits \setminus 200101\_SOU\_T5\_Renewal\_App \setminus Dehy \setminus SOU\_D2\_PTE \ (no\_combustor).ddf}$ 

Date: November 01, 2019

DESCRIPTION:

\_\_\_\_\_\_

Description: 40 MMscfd dehy unit; April '19 gas analysis,

gas temp, pressure and max glycol flow (3 Kim 20015); max gas flow, (no combustor)

Annual Hours of Operation: 8760.0 hours/yr

WET GAS:

\_\_\_\_\_\_

Temperature: 67.56 deg. F
Pressure: 409.70 psig
Wet Gas Water Content: Saturated

Component	Conc. (vol %)
Carbon Dioxide	4.6651
Methane	95.0269
Ethane	0.2657
Propane	0.0249
Isobutane	0.0054
n-Butane	0.0051
Isopentane	0.0012
n-Pentane	0.0003
Other Hexanes	0.0019
Methylcyclohexane	0.0005
Benzene C8+ Heavies	0.0001

DRY GAS:

Flow Rate: 42.0 MMSCF/day Absorber Stages: 1.3

LEAN GLYCOL:

Glycol Type: TEG
Water Content: 1.5 wt% H20
Flow Rate: 10.0 gpm

PUMP:

Glycol Pump Type: Gas Injection

Gas Injection Pump Volume Ratio: 0.080 acfm gas/gpm glycol

FLASH TANK:

Page: 2

Flash Control: Combustion device Flash Control Efficiency: 95.00 % Temperature: 100.0 deg. F Pressure: 30.0 psig



Models PV, SC

## **Product Bulletin**

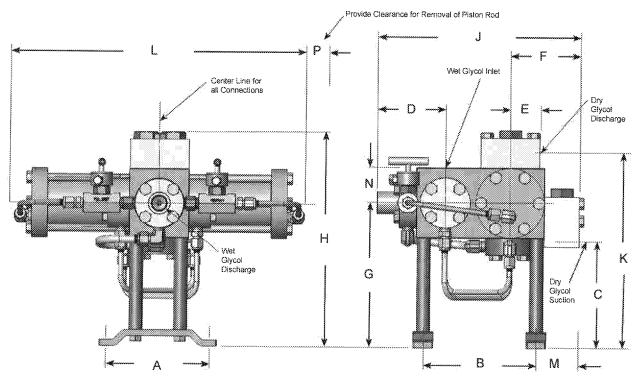


Figure 7

Table 3 - Glycol Pump Dimensions														
Model PV, SC	Α	В	С	D	E	F	G	Н	J	К	L	M	N	ρ
1720 PV	5 1/4 in.	5 11/16 in.	5 3/4 in.	5 7/16 in.	1 1/2 in.	3 1/2 in.	7 1/4 in.	10 7/8 in	10 3/16 in.	9 5/8 in.	15 in.	2 1/8 in.	1 3/4 in.	3 in.
	(133 mm)	(144 mm)	(146 mm)	(87 mm)	(38 mm)	(88 mm)	(184 mm)	(276 mm)	(258 mm)	(244 mm)	(381 mm)	(53 mm)	(44 mm)	(76 mm)
4020 FV & 2015 SC	5 1/4 in.	5 11/16 in.	5 3/4 in.	5 7/16 in.	1 1/2 in.	3 1/2 in.	7 1/4 in.	10 7/8 in.	10 3/16 in.	9 5/8 in.	15 in.	2 1/8 in.	1 3/4 in.	3 in.
	(133 mm)	(144 mm)	(146 mm)	(87 mm)	(38 mm)	(88 mm)	(184 mm)	(276 mm)	(259 mm)	(244 mm)	(381 mm)	(53 mm)	(44 mm)	(76 mm)
9020 PV & 5015 SC	6 1/4 in,	5 11/16 in.	6 3/8 in.	5 in.	1 3/4 in.	4 1/4 in.	8 3/4 in.	13 1/4 in.	13 7/8 in.	11 3/4 in.	20 in.	2 1/2 in.:	2 in .	3 in.
	(158 mm)	(144 mm)	(161 mm)	(127 mm)	(44 mm)	(107 mm)	(222 mm)	(336 mm)	(352 mm)	(289 mm)	(508 mm)	(63 mm)	(50 mm)	(76 mm)
21020 PV & 10015 SC	7 5/8 in.	10 1/8 ± 1/8	7 in.	5 3/8 in.	2 1/4 in	5 3/4 in.	9 1/4 in.	14 3/4 in.	16 5/8 in.	13 in.	24 in.	3 3/16 in.	2 1/2 in.	4 in.
	(193 mm)	(257 mm)	(177 mm)	(136 mm)	(57 mm)	(146 mm)	(234 mm)	(374 mm)	(422 mm)	(330 mm)	(508 mm)	(80 mm)	(63 mm)	(101 mm)
45020 PV & 20015 SC	10 3/4 in.	14 ± 1/8	9 in.	6 5/8 in.	2 5/6 in.	6 1/2 in.	11 3/8 in.	19 in.	21 1/8 in:	16 3/8 in.	34 in.	3 3/4 in.	3 1/2 in.	6 in.
	(273 mm)	(355 mm)	(228 mm)	(168 mm)	(66 mm)	(165 mm)	(288 mm)	(482 mm)	(536 mm)	(415 mm)	(863 mm)	(95 mm)	(86 mm)	(152 mm)

Table 4 - Glycol Pump Specifications								
Model Number	Max. G.P.M	Cap G.P.H	Size of Pipe Connections	Mounting Bolts	Approx. Weight	Max Strokes Per Minute	Glycol Output Strokes / Gal	Glycol Output Gal. / Strokes
1720 PV	67	40	1/2 in NPT (12 mm)	3/8 in. dia (9.42 mm)	66 lbs (29.93 kg)	40	59	0.017
4020 PV	.67	40	1/2 in NPT (12 mm)	. 3/8 in. dia (9.42 mm)	66 lbs (29.93 kg)	40	59	0.017
9020 PV	1,5	90	3/4 in NPT (19 mm)	1/2 in. dia (12 mm)	119 lbs (53,97 kg)	40	26.3	0.036
21020 PV	3,5	210	1 in NPT (25 mm)	1/2 in. dia (12 mm)	215 lbs (97.52 kg)	32	9	0.111
45020 PV	7,5	450	1 1/2 in NPT (38 mm)	1/2 in, dia (12 mm)	500 lbs (22.68 kg)	28	3.5	0.283
2015 SC	.33	20	1/2 in NPT (12 mm)	3/8 in. dia (9.52 mm)	66 lbs (29,93 kg)	55	147	0.0068
5015 SC	.63	50	3/4 in NPT (19 mm)	1/2 in. dla (12 mm)	119 lbs (53,97 kg)	50	52	0.019
10015 SC	1.67	100	1 in NPT (25 mm)	1/2 in. dia (12 mm)	215 lbs (97.52 kg)	48	25	0,040
2001580	3.03	200	1 1/2 in NPT (38 mm)	1/2 in. dia (12 mm)	500 lbs (22,68 kg)	40	8.8	0.114

## Heater & Reboiler Emission Calculations South Ignacio Central Delivery Point Red Cedar Gathering Company

Type Unit ID	TEG Reboiler RB1	TEG Reboiler RB2	Tank Heater H-101 & H-102	Catalytic Heater H-103
Unit Rating:	1.750 mmBtu/hr	0.750 mmBtu/hr	0.325 mmBtu/hr	0.008 mmBtu/hr
Fuel usage <sup>a</sup> :	1.944 mscf/hr	0.833 mscf/hr	0.361 mscf/hr	0.009 mscf/hr
	17.03 mmscf/yr	7.30 mmscf/yr	3.16 mmscf/yr	0.08 mmscf/yr
Operating hours:	8760 hr/yr	8760 hr/yr	8760 hr/yr	8760 hr/yr

<sup>&</sup>lt;sup>a</sup> Based on fuel heat content of: 900 Btu/scf (conservative estimate based on fuel gas analysis)

Criteria Polluta	nt Emissions		Potential Emissions (tpy)	Potential Emissions (tpy)	Potential Emissions (tpy)	Potential Emissions (tpy)
Pollutant	Emission Factor	Data Source	RB1	RB2	H-101 & H-102	H-103
$NO_X$	100.0 lb/MMscf	AP-42; Table 1.4-1	0.85	0.37	0.16	0.00
СО	84.0 lb/MMscf	AP-42; Table 1.4-1	0.72	0.31	0.13	0.00
PM <sub>10</sub>	7.6 lb/MMscf	AP-42; Table 1.4-2	0.06	0.03	0.01	0.00
SO <sub>2</sub>	0.6 lb/MMscf	AP-42; Table 1.4-2	0.01	0.00	0.00	0.00
VOC	5.5 lb/MMscf	AP-42; Table 1.4-2	0.05	0.02	0.01	0.00
CO <sub>2</sub>	120000.0 lb/MMscf	AP-42; Table 1.4-2	1022.00	438.00	189.80	4.67
Methane	2.3 lb/MMscf	AP-42; Table 1.4-2	0.02	0.01	0.00	0.00
CO₂e		18.20	927.59 MT/yr	397.54 MT/yr	172.27 MT/yr	4.24 MT/yr

Hazardous Air Pollu	itant (HAP) Emissio	ons	Potential Emissions (tpy)	Potential Emissions (tpy)	Potential Emissions (tpy)	Potential Emissions (tpy)	
Pollutant	Emission Factor <sup>b</sup>	Data Source	RB1	RB2	H-101 & H-102	H-103	
1,3-Butadiene	3.42E-04 lb/MMBtu	GRI Field Test Data	2.62E-03	1.12E-03	4.87E-04	1.20E-05	
2,2,4-Trimethylpentane	2.84E-03 lb/MMBtu	GRI Field Test Data	2.18E-02	9.33E-03	4.04E-03	9.95E-05	
Acetaldehyde	7.38E-04 lb/MMBtu	GRI Field Test Data	5.66E-03	2.42E-03	1.05E-03	2.59E-05	
Benzene	7.48E-04 lb/MMBtu	GRI Field Test Data	5.73E-03	2.46E-03	1.06E-03	2.62E-05	
Ethylbenzene	2.11E-03 lb/MMBtu	GRI Field Test Data	1.62E-02	6.93E-03	3.00E-03	7.39E-05	
Formaldehyde	8.44E-04 lb/MMBtu	GRI Field Test Data	6.47E-03	2.77E-03	1.20E-03	2.96E-05	
Methanol	9.64E-04 lb/MMBtu	GRI Field Test Data	7.39E-03	3.17E-03	1.37E-03	3.38E-05	
n-Hexane	1.8 lb/MMscf	AP-42; Table 1.4-3	1.53E-02	6.57E-03	2.85E-03	7.01E-05	
Styrene	2.08E-03 lb/MMBtu	GRI Field Test Data	1.59E-02	6.83E-03	2.96E-03	7.29E-05	
Toluene	1.02E-03 lb/MMBtu	GRI Field Test Data	7.82E-03	3.35E-03	1.45E-03	3.57E-05	
Xylene	1.32E-03 lb/MMBtu	GRI Field Test Data	1.01E-02	4.34E-03	1.88E-03	4.63E-05	
TOTAL HAPS			1.15E-01	4.93E-02	2.14E-02	5.26E-04	

b Uncontrolled emission factors for external natural gas combustion sources based on the highest emission factor between EPA's AP-42, GRI field data and GRI literature data sets, and the manufacturer's data.

### **Fugitive Emission Calculations**

Equipment count based fugitive emission approach using EPA's 1995 guidance for Oil and Gas Production Operations Table 2-4 emission factors

Facility:

**South Ignacio Central Delivery Point** 

#### **Engines/Compressors**

# of Engines:

# of cylinders per compressor: 12

#### **Total Facility Fugitive Emissions**

Average Gas Composition

Carbon Dioxide

Nitrogen Methane

Ethane

Propane

Isobutane

n-Butane

Isopentane

n-Pentane Cyclopentane

n-Hexane

Heptanes

Benzene

Toluene Ethylbenzene

Xylenes C8 + Heavies

Total VOC

Total HAP <sup>†</sup>

Total CO 2 e

Total Methane

Total CO ,

Cyclohexane

Other Hexanes

2,2,4-trimethylpentane

Methycyclohexane

Total vented Gas:

Mol %

4.6651

0.0000

95.0269

0.2657

0.0249

0.0054

0.0051

0.0012

0.0003

0.0000

0.0000

0.0000

0.0019

0.0000

0.0005

0.0000

0.0001

0.0000

0.0000

0.0000

0.0001

0.040

0.000

4.665

95.027

217.88 ton/yr

Ton/Yr

10.164

0.000

207.045

0.579

0.054

0.012

0.011

0.003

0.001

0.000

0.000

0.000

0.004

0.000

0.001

0.000

0.000

0.000

0.000 0.000

0.000

0.09

0.00

10.16

207.05

5,186.29

Components	Emission factor <sup>a</sup> (kg/hr/source)	Count	Total Emissions (lb/hr) 2.460				
Valves (gas)	0.0045	248					
Valves (light oil/liquid)	0.0025	160	0.882				
Pump seals (light oil)	0.013	0.013 64					
Other <sup>b</sup>	0.0088	272	5.277				
Pressure relief valves							
Connectors (gas)	0.00025	1408	0.776				
Open-ended lines <sup>c</sup>	0.0023	24	0.122				
Pneumatic Device Vents							
Total Emissions		***************************************	11.351				

#### Dehydrators

# of Dehys: 2

total # of glycol pumps: 5

Components	Emission factor <sup>a</sup> (kg/hr/source)	Count	Total Emissions (lb/hr)		
Valves (gas)	0.0045	56	0.556		
Valves (light oil/liquid)	0.0025	74	0.408		
Pump seals (gas)	0.0024	10	0.053 0.287		
Pump seals (light oil)	0.013	10			
Other <sup>b</sup>	0.0088	30	0.582		
Pressure relief valves					
Connectors (gas)	0.00025	352	0.194		
Open-ended lines <sup>c</sup>	0.0023	4	0.020		
Pneumatic Device Vents					
Total Emissions		***************************************	2.099		

## Station

# of Inlet Seperators:

1

# of engine/lube oil tanks: 8

Components	Emission factor <sup>a</sup> (kg/hr/source)	Count	Total Emissions (lb/hr)		
Valves (gas)	0.0045	79	7.837		
Valves (light oil/liquid)	0.0025	100	5.512		
Pump seals (gas)	0.0024	16	0.847		
Pump seals (light oil)	0.013	16	4.586		
Other <sup>b</sup>	0.0088	26	5.044		
Pressure relief valves					
Connectors (gas)	0.00025	251	1.383		
Open-ended lines <sup>c</sup>	0.0023	9	0.456		
Pneumatic Device Vents					
Total Emissions			25.665		

## **Compressor Blowdowns**

# of Compressors

8

Total Emissions	46.55	ton/yr
Density of Vented Gas <sup>n</sup>	0.05	lb/scf
Gas vented annually	1,920.00	Mscf/yr
Molecular weight of gas <sup>1</sup>	17.401	g/mol
Gas vented per blowdown <sup>e</sup>	20.0	Mscf/blowdown
Number of blowdowns <sup>d</sup>	96	blowdowns/yr

<sup>&</sup>lt;sup>a</sup> Emission factors from EPA's 1995 Protocol for Equipment Leak Emission Estimates, Table 2-4

b Derived from compressors, diaphragms, drains, dump arms, hatches, instruments, meters, pressure relief valves, relief valves and vents; applied to all equipment types other than valves, pump seals, connectors, or flanges.

<sup>&</sup>lt;sup>c</sup> Default component count from Table W-1B of Subpart W of 40 CFR Part 98

 $<sup>^{\</sup>rm d}$  Conservatively based on 12 blowdowns a year for each compressor

Conservative estimate using equation W-14a (40 CFR §98.233) and a 4,735 hp Caterpillar G3616LE plus an additional 2% for compressor starts

f Conservatively based on the April 2019 inlet gas analyses (this sample has the highest HAP and VOC content measured within the last year).

 $<sup>^{\</sup>rm h}$  Density of Gas (lb/scf) = 16.859 g/mol \* mol/22.4L \* lb/453.592g \*28.316L/scf = 0.05 lb/scf

<sup>&</sup>lt;sup>i</sup> Non-methane, non-ethane compounds

<sup>&</sup>lt;sup>i</sup> HAP emissions include benzene, toluene, ethylbenzene, xylenes, and n-hexane

## **Emissions Report - Summary Format** Tank Indentification and Physical Characteristics

Identification

User Identification: 500 bbi used oil tank City: Durango State: Colorado Company: Red Cedar

Vertical Fixed Roof Tank

Type of Tank: Description:

Tank Dimensions

Shell Height (ft): Diameter (ft): 20.00 13.25 Liquid Height (ft): 19.00 Avg. Liquid Height (ff): 10.00 Volume (gallons): 19,597.85 Turnovers: 12.00 Net Throughput(gal/yr): 235,174.20

Is Tank Heated (y/n):

Paint Characteristics

Shell Color/Shade: Gray/Medium Shell Condition Roof Color/Shade: Gray/Medium Roof Condition: Good

**Roof Characteristics** 

Type: Cone

Height (ft) 1.00 Slope (ft/ft) (Cone Roof) 0.00

Breather Vent Settings

Vacuum Settings (psig): Pressure Settings (psig) -0.03 0.03

Meterological Data used in Emissions Calculations: Alamosa, Colorado (Avg Almospheric Pressure = 11.19 psia)

## **TANKS 4.0.9d Emissions Report - Summary Format Liquid Contents of Storage Tank**

## 500 bbl used oil tank - Vertical Fixed Roof Tank Durango, Colorado

Liossid Daily Liquid Surf Bulk Tensperature (deg F) Tensp				Bulk	lk			Vagor Moi.	Liquid Mass	Vagor Mass	Mai.	Sasis for Vapor Pressure	
Mixture/Component	Month	Awg.	Mire.	ššan.	(deg F)	Awg.	Min.	\$68x.	Weight.	Fract.	Pract.	Weight	Calculations
Distillate fuel oil no. 2	A)}	51.78	37,44	66.07	44.16	9,0049	9.0031	0.0080	130,000G			188.00	Option 1: VP50 = .0045 VP60 = .0065

## **TANKS 4.0.9d Emissions Report - Summary Format** Individual Tank Emission Totals

## **Emissions Report for: Annual**

500 bbl used oil tank - Vertical Fixed Roof Tank Durango, Colorado

	Losses(lbs)									
Components		Breathing Loss	Total Emissions							
Distiliate fuel oil no. 2	3,53	6.38	9.91							

## **Emissions Report - Summary Format** Tank Indentification and Physical Characteristics

enterior of	tifiration	

User Identification: 95 bbl still vent tank City: Durango State: Colorado Company: Red Cedar

Type of Tank: Description: Vertical Fixed Roof Tank

**Tank Dimensions** 

Shell Height (ft): 3.00 Diameter (fl): Liquid Height (fl): Avg. Liquid Height (fl): Volume (gallons): 15.00 3.00 3,965.76 Net Throughput(gal/yr): 7,931.53 Is Tank Heated (y/n):

Paint Characteristics

Shell Color/Shade: Gray/Medium Good Gray/Medium Shell Condition Roof Color/Shade: Roof Condition: Good

Roof Characteristics

Cone Type:

Height (ft) 0.00 Stope (R/ft) (Cone Roof) 0.00

**Breather Vent Settings** 

Vacuum Settings (psig): 0.00Pressure Settings (psig) 0.00

Meterological Data used in Emissions Calculations: Alamosa, Colorado (Avg Almospheric Pressure = 11.19 psia)

## **TANKS 4.0.9d Emissions Report - Summary Format Liquid Contents of Storage Tank**

#### 95 bbl still vent tank - Vertical Fixed Roof Tank Durango, Colorado

,				Liquid									
Daily Liquid Sorf. Bulk							Vapos	Liquid	Vapor				
		Tem	perature (di	eg F)	Temp	Vapo	n Pressure	(psia)	%foi.	Mass	Mass	Nioi.	Basis for Vapor Pressure
Nixture/Component	Month	Aug.	hess.	ASSN.	(ಶ≋ಜ್ಞ F)	Avg.	Báin.	Wax.	Weight.	Fract.	Fract.	Weight	Calculations
Distillate fuel oil no. 2	All	51.76	37.44	68.07	44.16	6.0949	0.0031	0.0082	130,0000			188.00	Option 1: VP50 = .0045 VP60 = .0065

## **TANKS 4.0.9d Emissions Report - Summary Format** Individual Tank Emission Totals

## **Emissions Report for: Annual**

#### 95 bbl still vent tank - Vertical Fixed Roof Tank Durango, Colorado

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Distillate fuel oil no. 2	0.12	9.83	0.95

## **Emissions Report - Summary Format** Tank Indentification and Physical Characteristics

Identification

User Identification: 500 gal oil tank City: Durango State: Colorado Company: Type of Tank: Red Cedar Horizontal Tank Description:

Tank Dimensions Shell Length (ff): Diameter (ff): 5.00 4.00 Volume (gallons): 500.00 Turnovers: 24.00 Net Throughput(gal/yr): 12,000.00

Is Tank Heated (y/n): Is Tank Underground (y/n):

Paint Characteristics

Shell Color/Shade: Shell Condition Gray/Medium

Good

Breather Vent Settings

Vacuum Settings (psig): -0.03 Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: Alamosa, Colorado (Avg Atmospheric Pressure = 11.19 psia)

## **TANKS 4.0.9d Emissions Report - Summary Format Liquid Contents of Storage Tank**

## 500 gal oil tank - Horizontal Tank Durango, Colorado

200000000000000000000000000000000000000													
£ iquied													
		De	ily Dquid St	af.	Bulk				Vagor	Liquid	Vapor		
		Tem	pereture (de	eg (F)	Temp	Vapor Pressure (psia)		Refert.	Mass	Mass	8,658.	Basis for Vapor Pressure	
Mixture/Component	Month	Avg.	ક્ષકત.	Max.	(deg F)	Avg.	Min.	Mex.	Weight	Fract.	Fract.	Weight	Calculations
Distillate five oil on 2	431 441	51.76	37 44	86.07	48 18	2800.5	0.0034	0.0086	136 0000			188.06	Ontion 1: VPS0 = 0045 VPS0 = 0085

## **TANKS 4.0.9d Emissions Report - Summary Format Individual Tank Emission Totals**

## **Emissions Report for: Annual**

500 gal oil tank - Horizontal Tank Durango, Colorado

Losses(lbs)									
Components	Working Loss	Breathing Loss	Total Emissions						
Distillate fuel oil no. 2	0.18	0.18	0.36						

## Emissions Report - Summary Format Tank Indentification and Physical Characteristics

Identification

User Identification: 500 gal TEG tank
City: Durango
State: Colorado
Company: Red Cedar
Type of Tank: Horizontal Tank

Description:

Tank Dimensions

 Shell Length (ft):
 5.00

 Diameter (it):
 4.00

 Volume (gallons):
 500.00

 Turnovers:
 2.00

 Net Throughput(gal/yr):
 1,000.00

Is Tank Heated (y/n):
Is Tank Underground (y/n):

N

Paint Characteristics

Shell Color/Shade Gray/Medium Shell Condition Good

Breather Vent Settings

Vacuum Settings (psig): -0.03
Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations: Alamosa, Colorado (Avg Atmospheric Pressure = 11.19 psia)

## TANKS 4.0.9d Emissions Report - Summary Format Liquid Contents of Storage Tank

## 500 gal TEG tank - Horizontal Tank Durango, Colorado

***************************************					Liquid								
		Da	iliy Liquid S	urf.	≅u%				Vapor	Liquid	Vapor		
		Tem	perature (d	eg F)	Temp	Vapo	r Preseure	(psis)	Ma€.	Mass	Mess	Mici.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Min.	Max.	(deg F)	Avg.	Min.	Max.	Weight.	Frect	Fract.	Weight	Calculations
Triethylene Glycci	Aži	51.78	37.44	68.07	44.16	8,0008	9,9000	0.0000	150.1700			350.17	Option 2: A=7.18302007, B=2158.4581. C=185.92442

# TANKS 4.0.9d Emissions Report - Summary Format Individual Tank Emission Totals

## **Emissions Report for: Annual**

500 gal TEG tank - Horizontal Tank Durango, Colorado

Components	Working Loss	Breathing Loss	Total Emissions							
Triethylene Glycol	0.00	0.00	0.08							

## **Emissions Report - Summary Format Tank Indentification and Physical Characteristics**

Identification

500 gal TEG tank User Identification: City: Durango Colorado Red Cedar State: Company: Type of Tank: Horizontal Tank

Description:

Tank Dimensions Shell Length (ff): Diameter (ft): 5.00 4.00 Volume (gallons): 500.00 2.00 1,000.00 Turnovers: Net Throughput(gal/yr):

Is Tank Heated (y/n): Is Tank Underground (y/n):

Paint Characteristics

Shell Color/Shade: Gray/Medium Shell Condition Good

**Breather Vent Settings** 

Vacuum Settings (psig): -0.03 Pressure Settings (psig) 0.03

Meterological Data used in Emissions Calculations; Alamosa, Colorado (Avg Atmospheric Pressure = 11.19 psia)

## **TANKS 4.0.9d Emissions Report - Summary Format Liquid Contents of Storage Tank**

## 500 gal TEG tank - Horizontal Tank Durango, Colorado

					Liquid								
		Da	sily Liquid S	ust.	Bulk				Vapor	Liquid	Vapor		
		Tem	cerature (d	eg F)	Temp	Vapo	r Pressure	(psis)	88ai.	M355	Wass	Mos.	Basis for Vapor Pressure
Mixture/Component	Month	Avg.	Man.	Maor.	(deg F)	Avg.	Miss.	Max	Weight.	Fract.	Frect.	Weight	Calculations
Ethylene Glycol	All	53.78	37.44	86.07	44.16	0.0004	0.0002	0.0010	62.0700			82.97	Option 2: A=8.21211, B=2161.91, C=208.43

## **TANKS 4.0.9d Emissions Report - Summary Format Individual Tank Emission Totals**

## **Emissions Report for: Annual**

### 500 gal TEG tank - Horizontal Tank Durango, Colorado

	Losses(lbs)									
Components	Working Loss	Breathing Loss	Total Emissions							
Ethylene Głycol	0.00	0.01	0.01							